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## Amplitude and Period Effect on Heat Transfer in an Enclosure with Sinusoidal Heating from Below Using Lattice Boltzmann Method

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### ABSTRACT

This work presents a simulation of the phenomena of natural convection in an enclosure with a variable heating regime by the lattice Boltzmann method (LBM). We consider a square enclosure of side  $H$  filled with air ( $Pr = 0.71$ ) and heated from below, with a hot portion of length  $L = 0.8 H$ , by imposing a sinusoidal temperature. The unheated segments of the bottom wall are treated as adiabatic, and one of the vertical walls features a cold region, while the remaining walls remain adiabatic. The outcomes of the two-dimensional (2D) problem are depicted through isotherms, streamlines, the temperature evolution within the enclosure, and the Nusselt number. These visualizations span various amplitude values “ $a$ ” in the interval  $[0.2, 0.8]$ , and of the period  $T_0$  for  $Ra = 10^7$ . The amplitude and period effect on the results is evaluated and discussed. The amplitude of the temperature at the heart of the enclosure increases with the increase in amplitude. This also increases with the period ( $T_0$ ) of the imposed temperature, something that is not observable on the global Nusselt number.

### KEYWORDS

Sinusoidal heating; square cavity; lattice Boltzmann method; natural convection; heat transfer; under floor heating

### Nomenclature

|                        |   |
|------------------------|---|
| “ $a$ ”                | Amplitude   |
| $c_k$                  | Discrete Lattice velocities                                       |
| $D$                    | Dimension of space  |
| $F$                    | External buoyancy force   |
| $f_k(x, t), g_k(x, t)$ | Single particle distribution function for density and temperature |
| $\vec{g}$              | Gravity vector  |
| $H$                    | Height of the enclosure   |
| $L$                    | Heat portion length   |
| $Nu$                   | Nusselt number  |
| $Pr$                   | Prandtl number  |
| $Ra$                   | Rayleigh number   |



|                  |   |
|------------------|---|
| $T$              | Temperature                                       |
| $T_0$            | Period  |
| $t$              | Time  |
| $(u, v)$         | Macroscopic velocity                              |
| $(x, y)$         | Cartesian coordinates                             |
| $\alpha$         | Thermal diffusivity                               |
| $\beta$          | Coefficient of thermal expansion                  |
| $\Delta t$       | Lattice time step                                 |
| $\Delta x$       | Lattice space step                                |
| $\nu$            | Kinematic viscosity                               |
| $\omega_k$       | Weights factors                                   |
| $\rho$           | Fluid density                                     |
| $\theta$         | Dimensionless temperature $(T - T_c)/(T_h - T_c)$ |
| $\tau_m, \tau_s$ | Relaxation times for momentum and for scalar      |
| $c$              | Cold  |
| $h$              | Hot   |
| $k$              | Lattice link number                               |
| $opp$            | Opposite  |
| $s$              | Scalar  |
| $m$              | Momentum  |
| $eq$             | Equilibrium                                       |
| $max$            | Maximum   |

## 1 Introduction

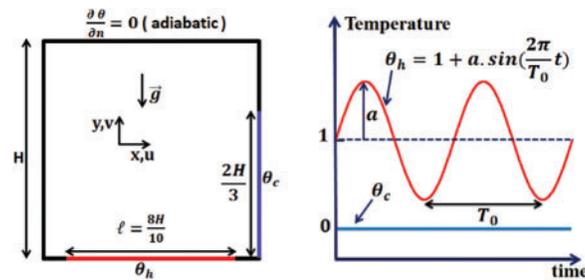
Natural convection is a widely observed phenomenon found in various systems, such as residential heating and cooling, heating circuits, and electronic devices [1–4]. Typically, this phenomenon arises from either variable or constant heating of a fluid. Many researchers have investigated and simulated such convection, employing diverse numerical methods to tackle complex problems (e.g., FDM: Finite Difference Method, FVM: Finite Volume Method, LBM: Lattice Boltzmann Method). A well-established benchmark solution for laminar natural convection of air within a square cavity was presented by de Vahl Davis [5]. Le Quéré [6] provided accurate solutions for a square cavity subjected to high Ra. Oliveira et al. [7] employed the FVM to address turbulent natural convection in square enclosures, incorporating large eddy simulation (LES). In their study, the lateral surfaces of the enclosure were maintained at different isothermal temperatures, while the upper and lower surfaces were thermally isolated. The investigation focused on  $Ra = 1.5810^9$ . Salat et al. [8] conducted a comparative result between experimental and numerical cases of turbulent flows in a differentially heated cavity. They demonstrated a good agreement between experimental results and numerical methods of mean temperature and vertical velocity. Numerous researchers have utilized the Lattice Boltzmann Method (LBM) to simulate various natural convection phenomena [9–13] and for complex geometry [14–17]. Some authors based on natural convection in the square enclosure, Mohamad et al. [18,19] evaluated LBM capability to simulate 2D natural convection in cavities by comparing LBM outcomes with those of FDM. They elucidated the necessary steps for utilizing LBM in natural convection problems. A comprehensive evaluation of forcing schemes within the lattice Boltzmann method (LBM) [20]. Rashidi [21] employed a proficient finite element approach to discretize the continuous system of depth equations, enabling the numerical simulation of shallow water wave propagation. Recent works by Abouricha et al. [22–25] adopted LBM to simulate natural convection in a square cavity

heated from below at a constant temperature. As the  $Ra$  increased, they observed a substantial rise in heat transfer, a pattern also observed in the heat source size ( $Lr$ ). For variable heating regimes, Abourida et al. [26] explored natural convection in a square cavity with horizontally heated walls subjected to different heating models, utilizing finite difference techniques. Their study encompassed a range of Rayleigh numbers ( $5 \times 10^5 \leq Ra \leq 10^6$ ) and revealed the influence of heating frequency on heat transfer, streamlines, and isotherms. They observed non-periodic solutions at higher Rayleigh numbers. Wang et al. [27] studied the impact of temperature-dependent properties on the natural convection of power-law nanofluids in rectangular cavities featuring sinusoidal temperature distributions. Nabwey [28] employed a set of analytical methods wherein the primary partial differential equations governing the flow were transformed into nonlinear ordinary differential equations (ODEs). This transformation was undertaken to investigate the heat and mass transfer characteristics of a non-Newtonian nanofluid flowing towards a vertically stretched surface. Most prior studies focused on cavities with heating walls maintained at constant (or periodically varying) temperatures or heat fluxes, employing numerical methods like FDM, FVM and FEM. Or based on the effect of physical or geometric parameters on the heat transfer [29–31]. Therefore, the current study aims to explore how varying the amplitude and period of heating temperature impacts heat transfer, flow structure, and temperature distribution within the cavity core using the simulation by lattice Boltzmann method (LBM), all while maintaining a fixed  $Ra$ .

## 2 Physical Configuration and Method

### 2.1 Physical Configuration

In this particular study, the LBM was employed to replicate the phenomenon of heat transfer through natural convection, incorporating the element of variable heating. The investigation revolves around a 2D enclosure (Fig. 1, left) filled with air characterized by a  $Pr = 0.71$ . The cavity, with a side length denoted as  $H$ , experiences heating from beneath, achieved by imposing a temperature denoted as  $\theta_h$  (Fig. 1, right) on a specific section measuring  $L = 0.8H$ , strategically positioned at the center of the lower wall. One of the vertical walls features a cold segment indicated by  $\theta_c = 0$ , whereas the remaining walls maintain adiabatic conditions. This configuration can simulate a small-scale test room (home shower), equipped with a solar water heater. The water circulating through the floor generates heat at varying temperatures over time, depending on the day and night.

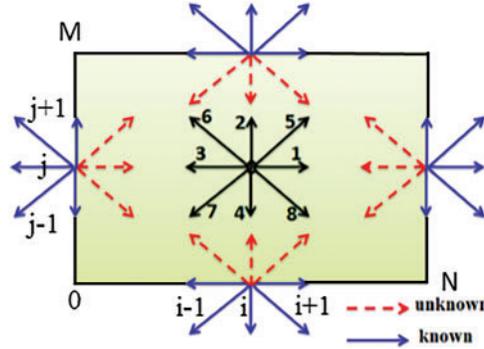


**Figure 1:** Physical geometry (left) and thermal excitations (right)

### 2.2 Lattice Boltzmann Method (LBM)

The LB framework utilized in this context aligns with the one applied in prior studies [22,24]. This model leverages a pair of distinct single-particle distribution functions:  $f_k(x, t)$  for addressing dynamic aspects and  $g_k(x, t)$  for simulating thermal fields. Hence, the approach corresponds to the

LBM referred to as model D2Q9, characterized by its two-dimensional nature and incorporation of nine discrete velocities, as illustrated in Fig. 2.



**Figure 2:** LBM model used D2Q9

The lattice Boltzmann equation under the BGK approximation and in the absence of external forces can be expressed as stated in references [22,32,33]:

$$\frac{\partial f_k}{\partial t} + c_k \frac{\partial f_k}{\partial x} = -\frac{1}{\tau_m} (f_k - f_k^{eq}) \quad (1)$$

The equilibrium distribution can be expressed mathematically by the following expression [34]:

$$f_k^{eq}(x, t) = \omega_k \rho(x, t) \left( 1 + 3 \frac{c_k u}{c^2} + \frac{9}{2} \frac{(c_k u)^2}{c^4} - \frac{3}{2} \frac{u^2}{c^2} \right) \quad (2)$$

where  $c = \frac{\Delta x}{\Delta t}$  is the lattice speed,  $\Delta x = 1$  is the lattice space, and  $\Delta t = 1$  is the lattice time.

For D2Q9 (Fig. 2), the discrete velocities  $c_k$  are defined as follows:

$$c_0 = (0, 0), c_{1-4} = (\pm 1, 0); (0, \pm 1) \text{ and } c_{5-8} = (\pm 1, \pm 1)$$

$$\text{The weights factors } \omega_k \text{ are given by: } \omega_0 = \frac{4}{9}, \omega_{1-4} = \frac{1}{9} \text{ and } \omega_{5-8} = \frac{1}{36}$$

Finally, the BGK approximation for the LB equation discretized and simplified with external forces can be written as:

$$f_k(x + c_k \Delta t, t + \Delta t) = (1 - w_m) f_k(x, t) + w_m f_k^{eq}(x, t) + \Delta t F_k \quad (3)$$

For momentum  $w_m$  is prescribed through kinematic viscosity as:

$$w_m = \frac{\Delta t}{\tau_m} = \frac{1}{3\nu + 0.5} \quad (4)$$

Taking into account the Boussinesq approximation, the external force denoted as  $F_k$  in Eq. (3) is expressed as follows:

$$F_k = 3\omega_k \frac{\rho g \beta \Delta T \cdot c_k}{c^2} \quad (5)$$

Finally, for the model D2Q9, the density  $\rho$  and velocity  $u$ , are calculated by summing moments within the velocity space as follows:

$$\rho(x, t) = \sum_{k=0}^{k=8} f_k(x, t) \quad (6)$$

$$\rho u(x, t) = \sum_{k=0}^{k=8} c_k f_k(x, t) \quad (7)$$

For the temperature, other distribution functions for the lattice Boltzmann method are defined as:

$$g_k(x + c_k \Delta t, t + \Delta t) = (1 - w_s) g_k(x, t) + w_s g_k^{eq}(x, t) \quad (8)$$

where  $w_s$  is associated to the diffusion coefficient as:

$$w_s = \frac{\Delta t}{\tau_s} = \frac{1}{3\alpha + 0.5} \quad (9)$$

The equilibrium distribution functions for the temperature can be used at first-order [35].

$$g_k^{eq} = \omega_k T(x, t) \left[ 1 + 3 \frac{c_k u}{c^2} \right] \quad (10)$$

The temperature  $T(x, t)$  is calculated by using the summation:

$$T(x, t) = \sum_0^8 g_k(x, t) \quad (11)$$

### 2.3 Boundary Conditions

The boundary conditions pertaining to the investigated problem are outlined below:

- Dynamic boundary conditions:

For all the walls:  $u = v = 0$

- Thermal boundary conditions:

The dimensionless temperature can be defined as:

$$\theta = \frac{T - T_c}{T_h - T_c} \quad (12)$$

On the adiabatic walls, we used this condition  $\frac{\partial \theta}{\partial n} = 0$ , where  $n$  is the normal of walls. The numerical approximation used for the top wall:

$$g_k(i, M) = g_k(i, M - 1) \quad (13)$$

Here,  $i$  denotes the iteration index along the  $x$  direction, while  $M$  signifies the count of lattice points situated on the upper wall as indicated in Fig. 2.

For the imposed temperature on the hot and the cold portion, the bounce-back conditions can be used:

$$g_k = (\omega_k + \omega_{opp(k)}) \theta - g_{opp(k)} \quad (14)$$

For example:  $(opp(1) = 3; opp(2) = 4; opp(6) = 8)$

On the cold portion:  $\theta_c = 0$

On the hot portion:  $\theta_h = 1 + a \cdot \sin\left(\frac{2\pi}{T_0} t\right)$

### 2.4 Nusselt Number

The Nusselt number at the hot part can be calculated by the expression below:

$$\overline{Nu} = \frac{-10}{8} \int_{\frac{1}{10}}^{\frac{9}{10}} \left. \frac{\partial \theta}{\partial y} \right|_{y=0} dx \quad (15)$$

### 3 Test of Numerical Method and Code

The FORTRAN code implemented in this study was validated and tested through a comparison of the outcomes against those reported by Le Quéré [6] for  $Ra = 10^7$ . Fig. 3 represents the configuration used for this validation. It is a differentially heated square cavity filled with air. In Table 1, a juxtaposition was made between the highest x-velocity value along the vertical midpoint ( $U_{max}$ ), the highest y-velocity value along the horizontal midpoint ( $V_{max}$ ), and the mean Nusselt number ( $\overline{Nu}$ ). The analysis of this comparison highlights a favorable concurrence, with a maximum discrepancy not surpassing 3.04%.

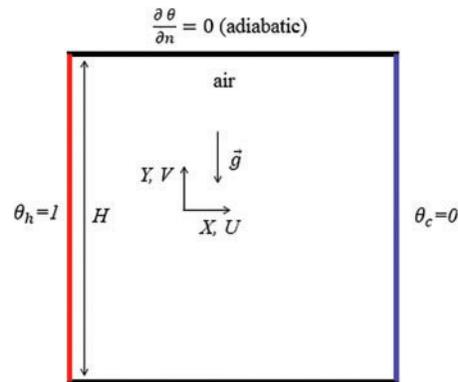


Figure 3: Square cavity differentially heated [6,36]

Table 1: Comparison between our results and those obtained by Le Quéré [6]

|                   | Results obtained | Le Quéré [6] | Deviation |
|-------------------|------------------|--------------|-----------|
| $U_{max}$         | 144.050          | 148.580      | 3.04%     |
| $Y$               | 0.878            | 0.879        |           |
| $V_{max}$         | 694.179          | 699.236      | 0.72%     |
| $X$               | 0.023            | 0.021        |           |
| $\overline{Nu}_h$ | 16.364           | 16.523       | 0.96%     |

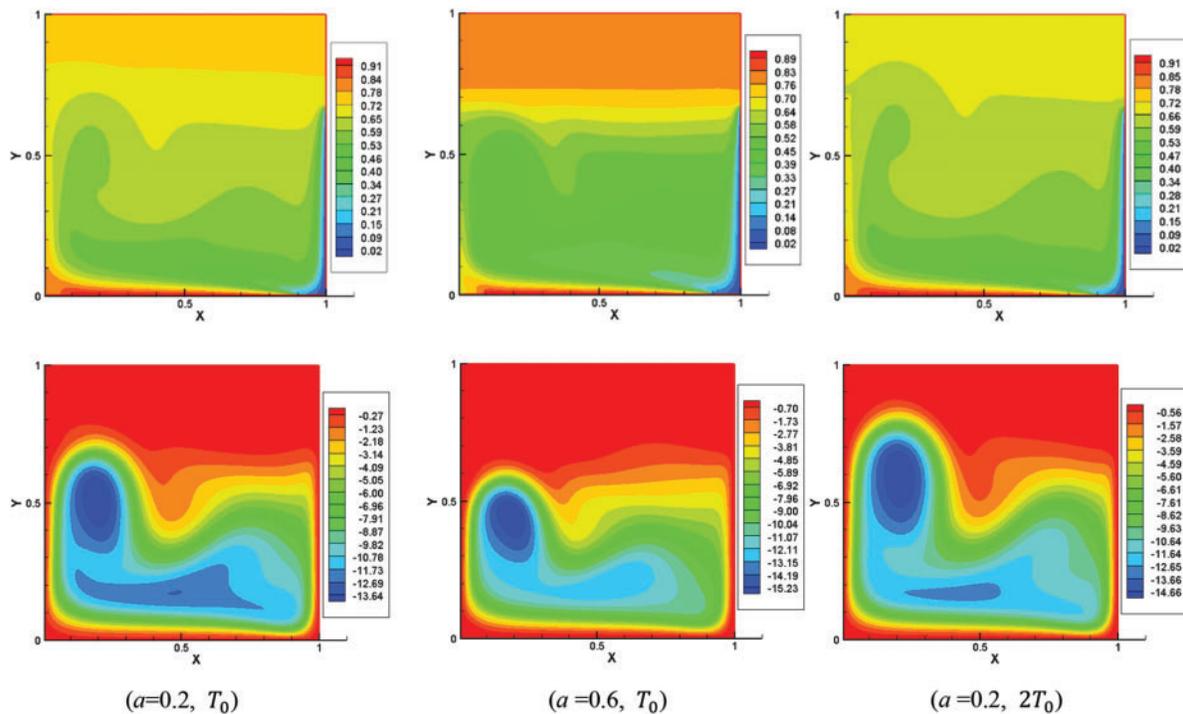
### 4 Results and Discussion

In the following section, the flow structures, temperature fields and heat transfer rates are inspected for divers values in the series of amplitude  $0.2 \leq a \leq 0.8$  and for double values of period  $T_0$  and  $T_0 = 2 \times T_0$ , by using air ( $Pr = 0.71$ ), a fixed Rayleigh numbers  $Ra = 10^7$ . Numerically in two dimensions, we have divided the physical domain into  $N = 210$  nodes along the x axis, and  $M = 210$  along the y axis. The stability of the numerical method used, the constraints of divergence code FORTRAN, and computing time are taken into consideration. We need the term  $g\beta$  figured in the expression of Rayleigh number,  $g\beta = Ra(\alpha\nu)/(\Delta TH^3)$ . Considering the lattice unit and the stability of the LBM, for example, we choose the kinematic viscosity  $\nu = 0.02$ , or another value less than 0.1. Based on the law of similarity and dimensionless numbers,  $Pr = 0.71 = \nu/\alpha$ , then the thermal diffusivity  $\alpha = 0.02/0.71$ . By replacing  $\Delta T$  by  $\Delta\theta$  and  $H$  by  $M$ , we can calculate  $g\beta = Ra(\alpha\nu)/(M^3)$  figured in Eq. (5).

Notice that the model is dimensionless, and all results will be presented in dimensionless forms and discussed in the last periods.

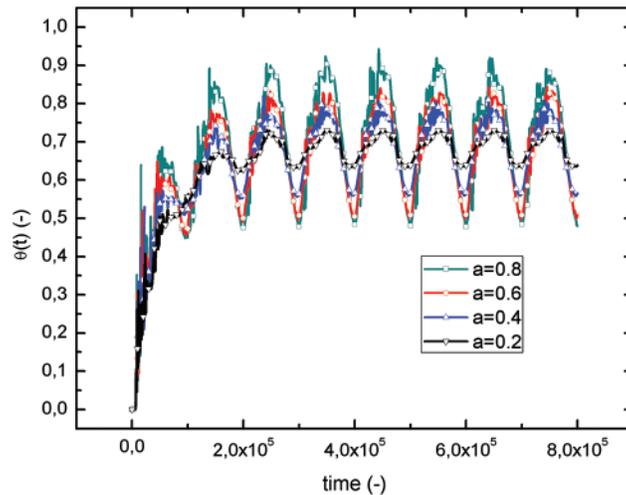
#### 4.1 Streamlines and Isotherms

The effect of the variation of the amplitude “a” on the thermal field and dynamic field is represented in Fig. 4, in the form of isotherms (above) and streamlines (below). We have examined the solution during one period  $T_0$  at  $t = nT_0 + T_0/i$ , where  $i = 1,2,3, \dots$  and  $n \geq 5$ . We notice that at every moment, we have a different solution by the fact that the imposed temperature varies as a sinusoidal function of time and can be minimal or maximum, which causes the change in the form of thermal field.

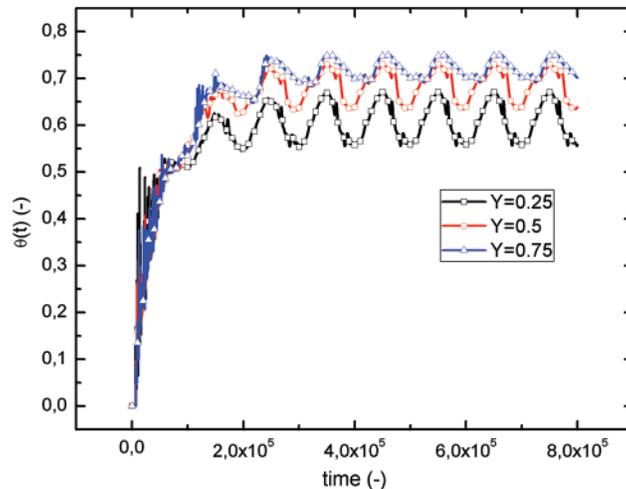


**Figure 4:** Isotherms (above) and streamlines (below) for the amplitude  $a = 0.2$  and  $a = 0.6$  at time calculation  $8.10^5$  steps

The examination of the isotherms shows that thermal stratification is generated near to the hot walls and at the top of the cavity when  $Y \geq 0.75$ , the dimensionless temperature is set around 0.71. Elevating both the amplitude and period results in an observed rise in temperature within the central region of the cavity, which is shown in Figs. 5 and 6. The examination of the streamlines shows that there is a dissymmetrical location of the cells and the flow is formed by a large cell contains small cells, more or less hot, rotates clockwise because the cold air decent near the right vertical wall pushing the hot air to continued rotation. Generally, the structure form of the flow does not change by the variation of the amplitude and the period, but it changes over time during a period  $t = n.T_0 + T_0/i$ .



**Figure 5:** Temperature evolution at the center ( $X = 0.5; Y = 0.5$ ) for various amplitudes “ $a$ ”



**Figure 6:** Evolution of temperature for different position along the vertical centerline  $X = 0.5$

Note that these figures are represented at the final instant of the calculation time  $8.10^5 = 8T_0 = 4T_0'$ . Apparently, at times  $t = nT_0$  and  $n = 5, 6, 7, 8$ , the change in isotherms and streamlines is very weak. On the other hand, at times  $t = nT_0 + T_0/i$  and  $i = 1, 2, 3, \dots$  there is a change but is not covered in this paper.

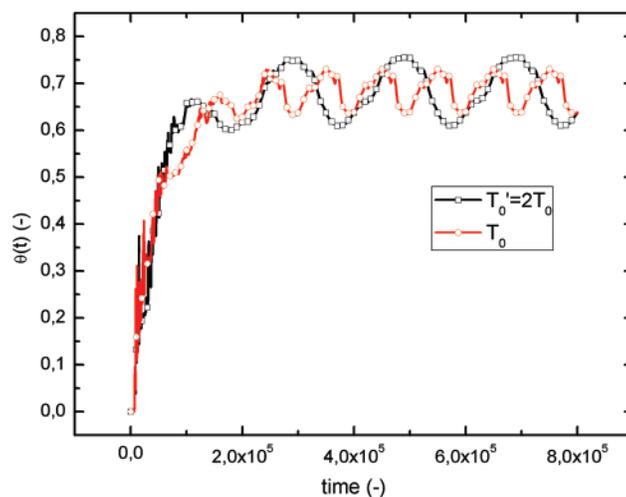
#### 4.2 Temperature Profiles

The temporal variations of dimensionless temperatures, denoted as  $\theta(t)$ , are depicted in Fig. 5 at the center of the enclosure for different values of the amplitude “ $a$ ” of the imposed temperature.  $\theta_h$ , and in Fig. 6 for the following positions  $Y = 0.25; 0.5; 0.75$  of the vertical mid plan  $X = 0.5$ , for an amplitude  $a = 0.2$ . Normally, the temperature at the heart of the cavity does not vary in phase with the imposed temperature. This is because of the time delay in heat transfer from one area to another.

For all values of the amplitude “ $a$ ” of the  $\theta_h$ , the dimensionless temperature  $\theta(t)$  at the center oscillates periodically around 0.66. Its amplitude increases with the increase of the amplitude “ $a$ ” and becomes disturbed for the reason of the turbulent flow in the center of the cavity. For the amplitudes 0.2 and 0.8, the temperature oscillates in the margin [0.63; 0.73] and [0.48; 0.88], respectively (Fig. 5). The examination shows that  $\theta(t)$  preserves the same periodicity with  $\theta_h$  and increases towards a maximum value when  $\theta_h > 1$  and decreases near a minimal value while  $\theta_h < 1$  due to the important hot air movement when  $\theta_h > 1$  that one has heating in this case and cooling in the other case  $\theta_h < 1$ .

Fig. 6 shows that the temperatures on the vertical medium axis for an amplitude  $a = 0.2$  oscillate periodically in the range [0.55; 0.75] around different mean values (0.61, 0.69 and 0.72 for  $Y = 0.25$ ,  $Y = 0.5$  and  $Y = 0.75$ , respectively). The oscillation amplitudes are very significant towards the bottom of the cavity and decrease as one goes upwards (when  $Y$  increases). When  $Y$  is superior strictly to 0.75, the evolution of  $\theta(t)$  approaches asymptotically towards very close values that appear in the upper third of the cavity, as already mentioned in the isothermal lines.

In Fig. 7, we present the evolution of  $\theta(t)$  at the center of the enclosures for the amplitude 0.2 and for double values of the period  $T_0$  and  $T_0' = 2 \times T_0$ , in directive to evaluate the period effect of  $\theta_h$  on the temperature inside the cavity. From these results, it is remarkable that the amplitude of  $\theta(t)$  at the center of the enclosures is affected by the period variation of  $\theta_h$ . It shows that the amplitude of  $\theta(t)$  at the center of the enclosures increases by increasing the period of  $\theta_h$ . This is due to the heating and cooling time, which increases for longer periods.



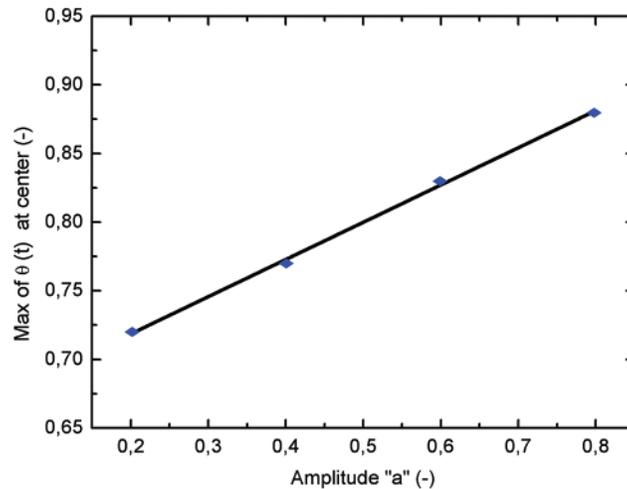
**Figure 7:** Period effect on temperature evolution at the center ( $X = 0.5$ ;  $Y = 0.5$ ) for  $a = 0.2$

The time evolution of the dimensionless temperature  $\theta(t)$  at the center of the square enclosures is shown in Fig. 8, for an amplitude of the imposed temperature in the range  $0.2 \leq a \leq 0.8$ . The temperature oscillates between a maximum  $\theta_{max}$  and minimum  $\theta_{min}$  around a mean value. This maximum

can be correlated with the amplitude “ $a$ ” in the linear form. After fitting the curve, for  $Ra = 10^7$  and  $0.2 \leq a \leq 0.8$ , the correlation between  $\theta_{max}$  And “ $a$ ” can be written as:

$$\theta_{max} = 0,27 \times a + 0,66 \quad (16)$$

This correlation gives an idea of the maximum temperature, or Expected temperature value at the center of the cavity for heating conditions already specified.

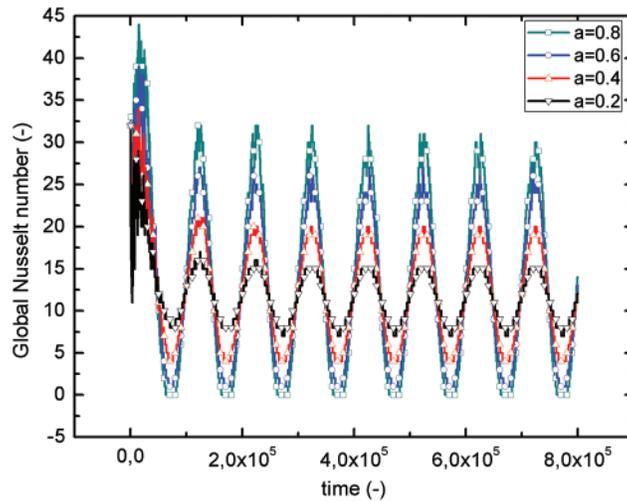


**Figure 8:** Maximum variation of the temperature at the center with amplitude “ $a$ ”

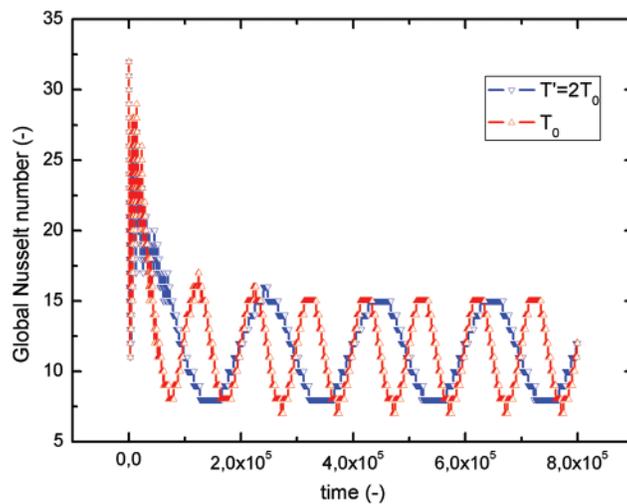
### 4.3 Heat Transfer

The investigation of heat transfer within the enclosures involves computing the Nusselt number ( $\overline{Nu}$ ) on the heated portion. The variation of this parameter is displayed in Fig. 9, for different values of amplitude “ $a$ ” and for double values of the period of  $\theta_h$ . In general, an increase in the amplitude “ $a$ ” leads to an enhancement in the heat transfer, as indicated by the Nusselt number within the enclosure. The evolution of  $\overline{Nu}$  continue periodic and oscillate in phase with  $\theta_h$  about a mean value equivalent to 12. We noticed that when “ $a$ ” increases the amplitude of  $\overline{Nu}$  similarly increases, this latter varied in the margin of  $7 \leq \overline{Nu}(t) \leq 15$  for  $a = 0.2$  and between of  $0 \leq \overline{Nu}(t) \leq 30$  for  $a = 0.8$ . We observed that when  $\theta_h$  maximal causes a disturbance of solution, unlike when this layer is minimal, that is due to the turbulent flow of air in the core of the enclosure, and its maximum is nearly doubled when “ $a$ ” doubled. Note well when  $\theta_h$  is minimal and the amplitude “ $a$ ” higher, the heat transfer does not exist as the amplitude  $a = 0.8$ .

Fig. 10 shows the temporal evolution of the  $\overline{Nu}$  for  $a = 0.2$ , and for two values of the period  $T_o$  and  $T_o' = 2 \times T_o$ . From these obtained results, it can be deduced that the amplitude of the Nusselt number ( $\overline{Nu}$ ) is not affected by the deviation of the period. But it keeps the same periodicity and always remains in phase with the imposed temperature  $\theta_h$ .



**Figure 9:** Amplitude “a” effect on global Nusselt number evolution on the hot portion



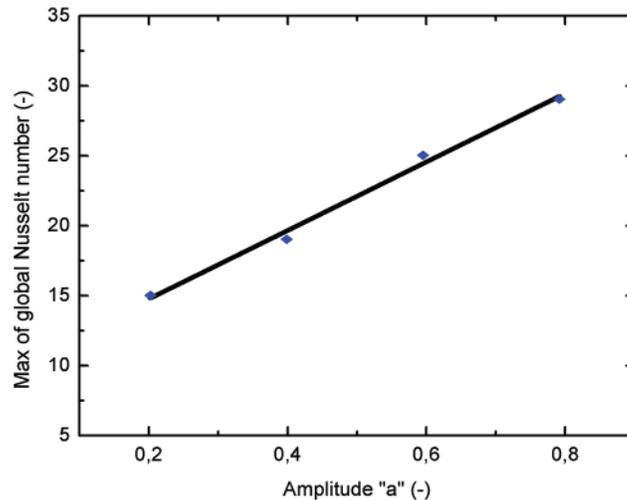
**Figure 10:** Period effect on global Nusselt number evolution on the hot portion for  $a = 0.2$

Generally, when heating is maintained at a constant temperature, during the steady-state phase, the temporal evolution of the average Nusselt number exhibits a consistent value for low Rayleigh numbers ( $Ra$ ). However, for higher  $Ra$  values, it tends to oscillate around a mean value. This is due to the appearance of the phenomena of transition to turbulence and the calculation method of Nusselt number  $\overline{Nu}$  (single or double precision). In this case, the number of  $Ra$  used is  $10^7$  and the heating is non-uniform. We observe at each step that there is a zigzag appearing in the evolution of the global Nusselt number represented in Figs. 8 and 9. Given that the number of calculation time steps is higher, the evolution appears as a trapezoidal wave.

The global Nusselt number oscillates around an average value with a maximum  $\overline{Nu}_{max}$  and minimum  $\overline{Nu}_{min}$ . For  $Ra = 10^7$  and in the range of the amplitude  $0.2 \leq a \leq 0.8$ , the maximum of the global Nusselt number  $\overline{Nu}_{max}$  varies linearly with “a”. After fitting the curve in Fig. 11, this relation can be written as:

$$\overline{Nu}_{max} = 24 \times a + 10 \quad (17)$$

This correlation is used to estimate the maximum of heat transfer in the enclosure for a well-determined heating rate.



**Figure 11:** Maximum variation of the global Nusselt number with amplitude “a”

## 5 Conclusion

In this article, we have conducted a numerical solution of heat transfer to analyze the effect of sinusoidal heating from below on the thermal field, dynamic field and Nusselt number  $\overline{Nu}$  by using the lattice Boltzmann method for  $Ra = 10^7$ . The Results found in this work show that:

- An increase in amplitude “a” increases the maximum of  $\theta(t)$  in the core of the enclosure and the heat transfer.
- Increasing the parameter “a” results in an amplification of the forces propelling the cells upwards, leading to the emergence of upward-moving air puffs that rotate around their own axes.
- The time evolution of  $\overline{Nu}$  continue periodic and oscillate in phase with  $\theta_h$  about a mean value.
- The variation of the period of  $\theta_h$  has a significant consequence on the amplitude of  $\theta(t)$  in the core of the enclosure; this end upsurges when the period “ $T_0$ ” increases.
- The Nusselt number  $\overline{Nu}$  is approximately not affected by the variation of the period “ $T_0$ ”.
- In the range of amplitudes  $0.2 \leq a \leq 0.8$  we have established the following correlations between the amplitude of the  $\theta_h$  and the maximum of  $\theta(t)$  at the center and the global Nusselt number:

For temperature:  $\theta_{max} = 0,27 \times a + 0,66$

For Nusselt number:  $\overline{Nu}_{max} = 24 \times a + 10$

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**Availability of Data and Materials:** Data will be made available on request.

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