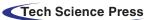


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ARTICLE





Preparation of Iron-Pillared Bentonite/Oyster Shell Composite and Phosphate Adsorption in Water

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ABSTRACT

Iron-pillared bentonite (FB) was prepared by Fe(III) modified bentonite, and then the composites (FB-OS) were prepared by iron-pillared bentonite and oyster shell powder. The composites were characterized by FTIR, SEM, TGA, and EDS, and the phosphorus removal test was carried out. The results showed that FB-OS contained a large amount of CaO. Its structure was compact, but there were gaps in it. The maximum bending stress and compressive strength were 43.7 N and 0.927 MPa, respectively. The phosphorus removal test showed that the phosphorus removal rate of FB-OS was more than 90%, and measured the maximum adsorption capacity was 48.31 mg/g. A large amount of spherical products were produced on the surface and inside of FB-OS after phosphorus removal, it was speculated that spherical products were amorphous calcium phosphate in the paper. Analysis indicated that there was chemical adsorption during phosphorus removal. The kinetic equation of phosphorus adsorption by FB-OS was $q_t = \frac{10.193t}{1+2.574t}$ (R² = 0.995). The adsorption rate was mainly controlled by outer film diffusion and intraparticle diffusion.

KEYWORDS

Oyster shell powder; iron-pillared bentonite; composite material; phosphorous removal

Nomenclature

OS	Oyster shell powder
CB	Calcium bentonite
FB	Iron-pillared bentonite
FB-OS	Iron-pillared bentonite/oyster shell powder composite material

1 Introduction

In the world, a large number of oysters are produced and consumed every year (South Korea and the United States produced 298,973 tons and 141,027 tons in 2016, respectively) [1], and then a larger



amount of oyster shells are produced. At present, most oyster shells are landfilled, occupying limited urban space and causing a waste of precious resources. The content of $CaCO_3$ in oyster shells is about 90%, and it also contains iron, magnesium, aluminum, and other trace metal elements, polysaccharides, and 16 kinds of amino acids [2,3]. It can be used in building materials, feed additives, and water treatment [4–6], among which water treatment has become a research hotspot due to its large dosage.

The oyster shell has a microporous structure and a large amount of CaCO₃, which can be combined with phosphorus in water to form more insoluble $Ca_3(PO_4)_2$, reducing the concentration of phosphorus in water [7]. However, the adsorption of natural oyster shell powder was slow, the adsorption capacity was low, and the concentration of phosphorus in water was still high after treatment [8,9]. Some scholars have modified it to enhance its phosphorus removal performance. According to the existing literature, the modification of oyster shell powder can be divided into three categories: thermal modification, metal compound modification, and clay modification. Thermal modification is to calcine at high temperatures. $CaCO_3$ in oyster shell powder was decomposed into CaO and CO₂ [10]. The products had good phosphorus removal performance, but the particle size was small and could easily lead to filter clogging (The solution after phosphorus removal was not colorless and transparent). In view of this shortcoming, some studies have introduced metal compounds to increase the particle size of precipitated particles. Metal compounds were mixed with calcined oyster shell powder (solid-solid) to produce composite materials for phosphorus removal. Flocculation performance of metal compounds could increase the particle size of the precipitated particles, commonly used iron, aluminum, Lanthanum, and other compounds in literature reports. Among them, iron and aluminum compounds modified oyster shell powder, Fe³⁺ and Al³⁺ in composite materials had strong flocculation performance, and Fe^{3+}/Ca^{2+} had synergistic effects in the phosphorus removal process. These methods increased the particle size of precipitated particles, and enhanced phosphorus removal performance [11,12]. About lanthanum compounds, La³⁺ had an antiinterference ability. Lanthanide compounds modified oyster shell powder could broaden the optimal pH range of solution to be treated [13]. The composite materials prepared by these methods had good phosphorus removal performance, and the precipitate particles became larger, but there were still a large number of fine precipitates, which cannot completely solve the problem of filter blockage caused by small particle size.

In order to further solve the problem of small particle size of precipitated particles, some scholars have studied the oyster shell powder by adding an additive with cohesiveness and plasticity, and then mixtures calcined to prepare a granular material. Bentonite as a clay has a wide source, large reserves, a certain degree of adhesion, plasticity, and ion exchange capacity [14], and it was commonly used in material preparation [15,16]. Materials made from bentonite often had good mechanical properties [17]. However, the adsorption performance of bentonite was not good. Some scholars have studied the way of pillaring metal ions such as Fe^{3+} , AI^{3+} , and Mg^{2+} to enhance their adsorption performance, and the phosphorus removal test achieved good results [18,19].

Regarding modification of oyster shell powder, the above analysis showed that thermal modification and metal compound modification could improve its phosphorus removal performance, and bentonite modification could obtain products with good mechanical properties. Can phosphorus removal materials with excellent performance be prepared if these modification methods were organically combined? After retrieval, there is no relevant literature reported. Therefore, the paper used metal compound pillaring technology to introduce iron ions to bentonite, and then iron-pillared bentonite was mixed with oyster shell powder, granulated and calcined to obtain granular materials. The samples were characterized by FTIR, SEM, TGA, and EDS, and the phosphorus removal test was carried out using an artificial phosphorus solution. The paper expects to use oyster shell waste to prepare phosphorus removal materials with good performance.

2 Experience

2.1 Materials and Instruments

Oyster shell powder (particle size is 120 mess, Yangxi Chengcun Haizhuzi Oyster Co., Ltd., Yangjiang, China); Calcium bentonite (particle size is 200 mess, Lingshou Dehang Mineral Products Co., Ltd., Shijiazhuang, China); Fe₂(SO₄)₃ (AR, Shanghai McLin Biochemical Technology Co., Ltd., Shanghai, China); NaOH (AR, Xilong Science Co., Ltd., Guangzhou, China); NaH₂PO₄·2H₂O (AR, Guangdong Guanghua Technology Co., Ltd., Guangzhou, China); Ascorbic acid (AR, Tianjin Damao Chemical Reagent Factory, Tianjin, China); (NH₄)₂MoO₄ (AR, Tianjin Baishi Chemical Co., Ltd., Tianjin, China); HCl (36%~38%, Shanxi Xinshunyuan, Jinzhong, China); Deionized water (laboratory homemade).

UV-5100B UV visible spectrophotometer (Shanghai Yuanxi Instrument Co., Ltd., Shanghai, China); TGA2 synchronous thermal analyzer (TA, New Castle, USA); EVO18 scanning electron microscope (Zeiss, Oberkochen, Germany); BSX2-5-12P muffle furnace (Shanghai Yiheng Technology Co., Ltd., Shanghai, China); Spectrum 100 FTIR (Perkin Elmer Inc., Waltham, USA); Hand-shaking granulator (Shanghai Zhenyue Trading Co., Ltd., Shanghai, China).

2.2 Sample Preparation

(1) Preparation of iron-pillared bentonite

According to the literature and slightly improved [20], the preparation method of iron-pillared bentonite was as follows: The iron-pillared liquid was prepared by n (OH⁻): n (Fe³⁺)=1: 1.5. 100 g calcium bentonite was dispersed into 2.0 L deionized water, and the iron-pillared liquid was added to the calcium bentonite solution to reach 10 mmol/g. The other operations (such as filtering, washing, and drying) were the same as those in the literature, and the iron-pillared bentonite (FB) was finally obtained.

(2) Preparation of iron-pillared bentonite/oyster shell composite

The oyster shell powder and iron-pillared bentonite were fully mixed at a mass ratio of 3:1 (B-FB-OS). An appropriate amount of deionized water was added into mixed powder to get muddy solid. The muddy solid granulated by hand-shaking granulator (cylinder diameter 5 mm, height $6\sim7$ mm) to obtain granular materials. The granular materials dried at 105°C for 1 h, and then transferred to a muffle furnace at 11°C/min to 700°C and held for 1 h. Naturally cooling in the muffle furnace, the composites iron-pillared bentonite/oyster shell powder composite (FB-OS) were finally obtained.

2.3 Sample Characterization

(a) Fourier transform infrared spectroscopy (FTIR)

The sample to be tested was added with KBr powder, pressed, and scanned at $450 \sim 4000 \text{ cm}^{-1}$ band.

(b) Thermal stability analysis (TGA)

The temperature program was set (temperature range of $40^{\circ}\text{C}-800^{\circ}\text{C}$, nitrogen heating rate of 10°C/min). $3\sim5$ mg sample was placed in the instrument. Temperature programmed to obtain TGA, and DTG obtained by TGA mathematical processing.

(c) Scanning electron microscope (SEM)

After the pretreatment of the sample to be tested, it was placed in the instrument, and the high-energy particles impacted the surface to observe the surface morphology of the sample.

(d) Energy dispersive spectrometer (EDS)

The composition and content of elements in the sample were analyzed by using the characteristic energy of X-ray photons of different elements.

(e) Determination of particle strength

The samples were placed on the instrument and compressed from top to bottom until the particles were damaged. The maximum bending stress was recorded and paralleled for 15 times. The compressive strength σ_c (Pa) was calculated by formula (1).

$$\sigma_c = \frac{2 \cdot F}{\pi \cdot T \cdot L} \tag{1}$$

where T(m) is the diameter of the cylinder; L(m) is the length of the cylinder; F(N) is the maximum bending stress.

2.4 Phosphorus Removal Test

(1) Operation process

Standard phosphorus solution (5.00 g/L) was prepared. Phosphorus solutions of other concentrations (5~150 mg/L) were prepared by diluting with 5.00 g/L standard phosphorus solution in the experiment.

The phosphorus removal performance test of composite materials was as follows: The phosphorus solution was added to a glass reagent bottle. FB-OS was added into above solution, and FB-OS statically adsorbed phosphorus from solution in a constant temperature water bath. Test water samples were taken at $3\sim5$ cm below the liquid level on time, and they filtered by 0.45 µm filter membrane. The concentrations in the filtrate were determined. Single factor experiments were carried out on adsorption time, water bath temperature, amount of adsorption materials and different initial concentrations of phosphorus.

(2) Determination of phosphorus content in solution

The content of phosphorus in water was determined by HCl-ammonium molybdate-spectrophotometer method according to the literature [21]. The standard curve of phosphorus concentration was obtained: A = 0.00211c + 0.000292683 (R²=0.9996), where A is absorbance and c is phosphorus concentration (mg/L).

(a) Phosphorus removal rate

$$R = \frac{c_t}{c_0} \times 100\% \tag{2}$$

where R (%) is the removal rate of phosphorus; c_0 and c_t (mg/L) are the initial phosphorus concentration and t (h) concentration, respectively.

(b) Phosphorus adsorption capacity

$$q = \frac{(c_0 - c_t)V}{m} \tag{3}$$

where $q \pmod{g}$ is the adsorption amount of phosphorus; V(L) is the volume of phosphorus solution; m(g) is the mass of the sample.

2.5 Adsorption Kinetic Equation

In order to explore the adsorption behavior of FB-OS, pseudo-first-order kinetics and pseudo-secondorder kinetics equations were fitted for its adsorption curve [22–24]. The equation was as follows: Pseudo-first-order kinetics equation (PFO) [25]:

$$q_t = q_e \left(1 - e^{-k_1 t} \right) \tag{4}$$

The logarithm of formula (4) is transformed into:

$$lg(q_e - q_t) = lg(q_e) - \frac{k_1 t}{2.303}$$
(5)

Pseudo-second-order kinetic equation (PSO) [25]:

$$q_t = \frac{q_e^2 k_2 t}{1 + q_e k_2 t} \tag{6}$$

Formula (6) is transformed into:

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e}$$
(7)

where q_e and q_t (mg/g) are the adsorption capacity of the adsorbent at equilibrium; t (h) is adsorption time; k_I (h⁻¹) and k_2 (g/(mg·h)) are rate constants.

3 Result

3.1 Characterization of Materials

3.1.1 FTIR Results and Analysis

Fig. 1 is the infrared spectra of raw materials and products. According to the figure, both calcium bentonite and iron-pillared bentonite contained the characteristic peaks of 2829 cm⁻¹ (-CH₃ symmetrical stretching vibration peak) and 1367 cm⁻¹ (C-H bending vibration peak). Among them, calcium bentonite also contained the characteristic peak of 2740 cm^{-1} (-CH₂ symmetrical stretching vibration peak), and iron-pillared bentonite had the characteristic peaks of 2952 cm⁻¹ (-CH₃ asymmetric tensile vibration peak) and 2660 cm⁻¹ (-CH₂ symmetrical stretching vibration peak) [26]. The above proved that calcium bentonite and iron-pillared bentonite both contained organic matter, and showed that the iron-pillared modification process did not completely wash away the original organic matter of calcium bentonite. Meanwhile, calcium bentonite and iron-pillared bentonite also contained 1105 cm⁻¹ (Si-O stretching vibration peak in quartzite), 1034 cm⁻¹ (Si-O stretching vibration peak), 508 cm⁻¹ (low-frequency Si-O vibration), and 472 cm⁻¹ (Si-O-Fe bending vibration peak) characteristic peaks, indicating that both contained SiO₂ and Fe₂(SiO₃)₃ [27]. Compared with calcium bentonite, iron-pillared bentonite had several obvious differences. Iron-pillared bentonite had 618 cm⁻¹ (Si-O-Al bending vibration peak) and 1443 cm⁻¹ (CO₃²⁻ stretching of calcite) characteristic peaks, on the base of the reports [28,29], which explained that iron-pillared bentonite contained $Al_2(SiO_3)_3$ and $CaCO_3$. The iron-pillared bentonite formed an obvious characteristic absorption peak of $Fe(OH)_3$ hydroxyl group at 771 cm⁻¹, which was the most obvious difference with calcium bentonite. Combined with the literature analysis, this may be caused by the intercalation of Fe(III) in the iron-pillared liquid into the bentonite interlayer during the modification of calcium bentonite [30,31]. It evidenced that the iron-pillared bentonite was successfully prepared in this experiment. Fig. 1 also showed that oyster shell powder had characteristic peaks of 2752 cm⁻¹, 1443 cm⁻¹, 1034 cm⁻¹, and 870 cm⁻¹ (Ca-O stretching vibration peak), which explained that oyster shell powder contained organic matter, SiO₂, and CaCO₃ [31,32]. This was because of the contamination from impurities such as soil or cement during oyster farming, and oyster shell pretreatment did not completely remove impurities, resulting in oyster shell powder containing SiO₂. FB-OS (Fig. 1) had characteristic peaks of 2952 cm⁻¹, 2829 cm⁻¹, 2714 cm⁻¹, and 1367 cm⁻¹. This expressed that there was still incompletely decomposed organic matter in the particles after calcination. FB-OS also contained

1135 cm⁻¹, 963 cm⁻¹ (Al-Al-OH), 870 cm⁻¹, 711 cm⁻¹ and 534 cm⁻¹, meaning that FB-OS also contained CaO, CaCO₃, Al₂O₃, MgO and SiO₂. FB-OS did not form a new characteristic peak. However, in the literature [33], CaO produced by the decomposition of oyster shell powder reacted with SiO₂ to form CaSiO₃ at high temperatures. This may produce too little CaSiO₃ to be shown in Fig. 1. In summary, the organic matter was not completely decomposed during the calcination process, and Fe(III) was successfully embedded into the calcium bentonite interlayer, and some oyster shell powder was pyrolyzed to generate CaO at high temperature.

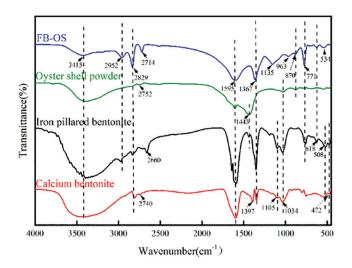
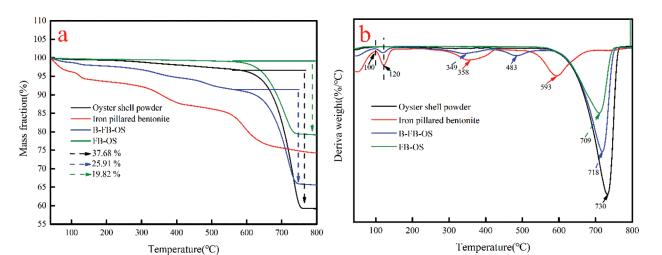


Figure 1: FTIR of calcium bentonite, iron-pillared bentonite, oyster shell powder and FB-OS

3.1.2 Results and Analysis of TGA and DTG

The thermal analysis of oyster shell powder, iron-pillared bentonite, B-FB-OS, and FB-OS was carried out, and the results were shown in Figs. 2a, 2b. Weight loss before 100°C was caused by each substance's volatilization of free water [34]. A small weight loss peak was formed near 120°C, this was attributed to the volatilization of bound water in iron-pillared bentonite and B-FB-OS at high temperatures [35]. B-FB-OS had a small weight loss peak near 349°C, and iron-pillared bentonite also had a small weight loss peak at 358°C. According to the literature [36], this peak was the dehydration of -OH and -COOH in organic matter at high temperatures. This indicated that iron-pillared bentonite contained organic matter. B-FB-OS had a small weight loss peak near 483°C, and iron-pillared bentonite also had a small weight loss peak at 593°C. These peaks were the weight loss peak of Fe(OH)₃ and Al(OH)₃ removing H₂O to form Fe₂O₃ and Al_2O_3 at high temperatures [36,37]. Among them, the ratio of impurity in the sample might be effecting the dehydration temperature of Al(OH)₃ and Fe(OH)₃ in the sample during calcination [38,39]. Thus, dehydration temperature of metal compounds decreased in B-FB-OS. Oyster shell powder, B-FB-OS and FB-OS had a significant weight loss peak at 730°C, 718°C and 709°C, respectively, which was due to the mass loss caused by the thermal decomposition of CaCO₃ in oyster shell powder into CaO and CO₂. The weight loss peak temperature of CaCO₃ in B-FB-OS and FB-OS was lower than that of oyster shell powder because of the presence of metal ions such as Al³⁺ in clay, Al³⁺ promoted the decomposition of CaCO₃ [40-42]. The difference between B-FB-OS and FB-OS may be caused by the different relative content of Al³⁺. The temperature of water volatilization and organic matter decomposition was lower than 560°C. Above 560°C, only CaCO₃ decomposition led to weight loss. At 560°C~800°C, the weight loss rates of oyster shell powder, B-FB-OS and FB-OS were 37.68%, 25.91%, and 19.82%, respectively. The weight loss rate of FB-OS was compared with that of oyster shell powder and B-FB-OS, which explained that only part of CaCO₃ decomposed during the calcination process, and



a large amount of undecomposed CaCO₃ remained in the composite. In conclusion, there was decomposition of organic compounds, dehydration of metal hydroxides, and CaCO₃ pyrolysis in the process of calcination.

Figure 2: Thermogravimetric analysis diagram (a is the TGA diagram of raw materials and products, b is the DTG diagram of raw materials and products)

3.1.3 Results and Analysis of SEM and EDS

Fig. 3 is the SEM diagram of calcium bentonite, iron-pillared bentonite and FB-OS before and after phosphorus removal. It can be seen that there was a leaf-like texture on the surface of calcium bentonite, and calcium bentonite was composed of leaf-like blocks [43]. The iron-pillared bentonite (Fig. 3b) was also a leaf-like stacking structure, which showed that the effect of modification on the structure of calcium bentonite was not significant. In order to further explore the element composition of iron-pillared bentonite, its SEM diagram (Fig. 3b) was analyzed by EDS, and the results were shown in Fig. 4a. The characteristic peaks of Fe, C, O, Na, Al, S, Mg, K, Si and Ca were observed on EDS. The characteristic peaks of C, S, and O indicated that iron-pillared bentonite contained organic matter. The characteristic peak of Si proved that iron-pillared bentonite contained SiO_2 . The characteristic peaks of K, Mg, Ca, Al, Fe, and Na indicated that iron-pillared bentonite contained a variety of minerals. In particular, Fig. 4b showed that the weight percentage of iron in iron-pillared bentonite was 24.67%. According to the literature [44], the highest weight percentage of Fe₂O₃ in calcium bentonite was about 8.6%. Relatively speaking, the iron content in the iron-pillared bentonite had been significantly improved, which indicated that some Fe(III) may be successfully embedded in the interlayer of calcium bentonite.

Fig. 3c showed that the FB-OS structure was compact but with gaps. The compact structure of FB-OS was due to the good plasticity and adhesion of iron-pillared bentonite, it made up for the disadvantage that oyster shell powder cannot be formed. In addition, the compact structure was one of the reasons why the composite material had good mechanical properties. The maximum bending stress of FB-OS measured by the particle strength tester was 43.7 N and the compressive strength was 0.927 Mpa. Of course, iron-pillared bentonite also contributed to the mechanical properties of the material. Needle-like crystals could be observed inside the material (Fig. 3d). According to the literature [33,45], it was speculated that needle-like crystals may be goethite or hydrated calcium silicate. However, the characterization results of this paper failed to confirm which substance it was, so the structure needs further research and analysis. After phosphorus removal, a large number of spherical products were formed on the surface of FB-OS (Fig. 3d), and they were characterized by EDS. The EDS results showed that the spherical products

contained C, K, Mg, Na, Ca, O, Fe, Al, S, P and Si elements (Fig. 4c), and the mass percentages of Ca, O and P were 19.51%, 30.02% and 4.04%, respectively (Fig. 4d). On based of the literature [46,47], amorphous calcium phosphate was composed of Ca, O and P elements, and its morphology under electron microscope was spherical. Based on the above analysis, it was speculated that the spherical product was amorphous calcium phosphate in this experiment. This indicated that PO_4^{3-} (HPO_4^{2-} and H_2PO^-) in phosphorus solution reacted with Ca^{2+} to form Ca_3 (PO_4)₂ (CaHPO₄ and Ca(H_2PO_4)₂), and the products adhered to the surface of the adsorbent. The spherical product also contained C, Fe, Al, S, K, Na, Mg, and Si elements. It was possible that the amorphous calcium phosphate was doped with FePO₄, AlPO₄ and iron-pillared bentonite during the formation. Spherical products could also be observed inside FB-OS (Fig. 3e), which was the same as the spherical products on the surface (Fig. 3d). This showed that phosphorus could enter into the interior of the composite material along the gap during the phosphorus removal process, and reacted with Ca²⁺ to form amorphous calcium phosphate.

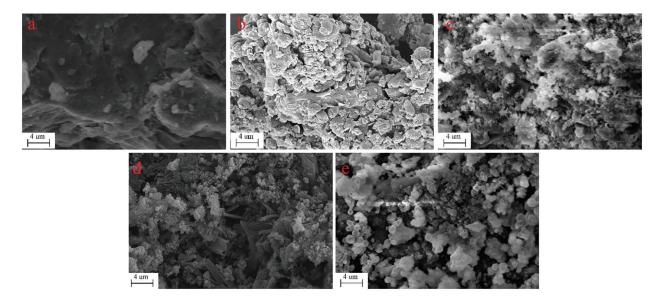


Figure 3: SEM of each substance (a is calcium bentonite, b is iron-pillared bentonite, c is the internal structure of FB-OS before phosphorus removal, d is the surface structure of FB-OS after phosphorus removal, e is the internal structure of FB-OS after phosphorus removal)

3.2 Phosphorus Adsorption Experiment

3.2.1 Effect of Temperature on Phosphorus Removal Performance of FB-OS

Fig. 5a showed the results of different temperatures on the phosphorus removal performance of FB-OS. The experimental conditions were an initial phosphorus concentration of 150 mg/L and a water volume of 50 mL. Before 5 h, the figure showed that although the adsorption rate at 40°C was higher than that at 30°C, the difference between the two could be ignored, and they were slightly higher than 20°C. This was because the increase of temperature accelerated the movement of ions in the system, which increased the contact probability between PO₄³⁻ and the active sites. That was conducive to the adsorption of phosphorus by FB-OS [48]. After 5 h, the adsorption of phosphorus by FB-OS tended to be at equilibrium under three temperature conditions. At 30 h, the adsorption capacities at 20°C, 30°C and 40°C were 3.48, 3.69 and 3.65 mg/g, respectively. At this time, the phosphorus removal rates all were higher than 90%. Based on the above analysis, under the experimental conditions, high temperature could accelerate the adsorption of phosphorus by FB-OS, but the increase was not significant, and the

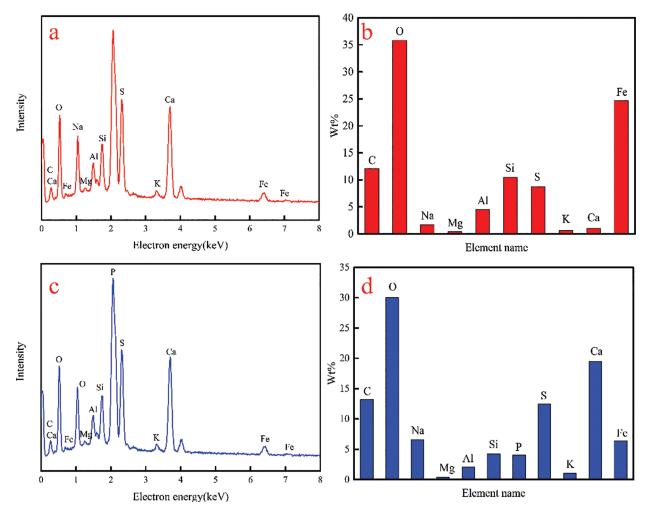


Figure 4: Electron diffraction spectra of iron-pillared bentonite and spherical products (a, b are EDS of iron-pillared bentonite, c, d are EDS of spherical products)

3.2.2 Effect of FB-OS Dosage on Phosphorus Removal Performance

At room temperature, different amounts of FB-OS were added to 200 mL aqueous solution with an initial phosphorus concentration of 150 mg/L, and test water samples were taken after 2 d. The results were shown in Fig. 5b. As can be seen from the figure, the influence of FB-OS dosage on phosphorus adsorption could be roughly divided into two situations: $0\sim3$ g and above 3 g. The dosage of FB-OS was $0\sim3$ g. With the increase of FB-OS dosage, the active center increased, Ca^{2+}/PO_4^{3-} increased, the probability of Ca^{2+} contacting with PO_4^{3-} (HPO₄²⁻ and H₂PO₄⁻) increased, and the removal rate increased [11,49]. The amount of adsorbent was 3 g, and the phosphorus removal rate reached 99.46%. When FB-OS was further increased, the dosage was greater than the demand for phosphorus removal, and the phosphorus removal rate was no longer significantly improved. Therefore, the optimum dosage of FB-OS was 99.46%.

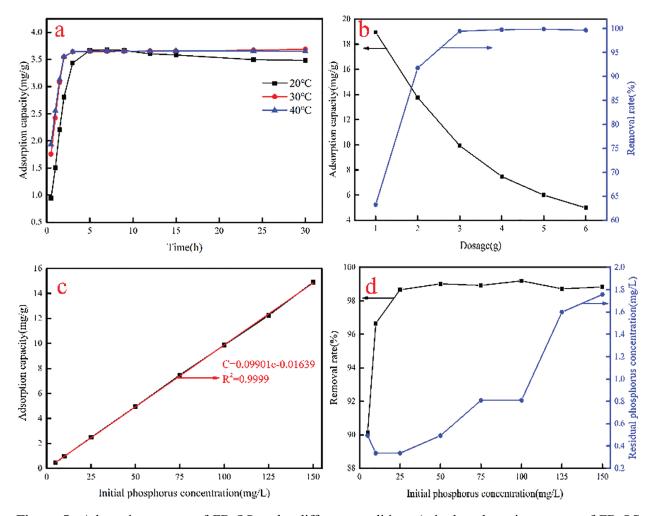


Figure 5: Adsorption curves of FB-OS under different conditions (a is the adsorption curves of FB-OS under different temperatures, b is the adsorption curves of FB-OS under different dosages, c is the absorption curves of FB-OS under different phosphorus concentration, d is the removal rate and residual phosphorus concentration curves of FB-OS under different phosphorus concentration)

3.2.3 Effect of Different Phosphorus Concentrations on Adsorption Properties of FB-OS

Phosphorus solution (250 mL 300 mg/L) was prepared, and 1.0 g FB-OS was added into above solution. At room temperature, FB-OS statically adsorbed phosphorus from solution. After 14th, 15th, and 16th days, phosphorus concentration in the solution was almost the same. The maximum adsorption capacity of the sample was calculated to be 48.31 mg/g.

In order to study the effect of different initial phosphorus concentrations on the phosphorus removal effect of FB-OS, 100 mL of aqueous solution with different phosphorus concentrations was prepared, 1.0 g FB-OS was added into above phosphorus solution, at room temperature FB-OS statically adsorbed, test water samples were taken after 2 d, and phosphorus concentration was measured, the results were shown in Fig. 5c. The figure showed that under the experimental conditions, the adsorption capacity increased linearly with the phosphorus concentration increasing. This was due to FB-OS having sufficient active sites, PO_4^{3-} was more, the probability of contact with the active site was greater, and the adsorption capacity of FB-OS was greater [50]. Fig. 5d also showed that the removal rate increased first

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and then remained unchanged with the increase of initial phosphorus concentration. The removal rates of all experiments were in the range of 90.14%~99.19%. When the phosphorus concentration was $5\sim100 \text{ mg/L}$, the phosphorus concentration was less than 1 mg/L after phosphorus removal. And $100\sim150 \text{ mg/L}$, residual phosphorus was $1.60\sim1.76 \text{ mg/L}$. Increase in the adsorbent, the residual phosphorus concentration was expected to be reduced to 1 mg/L. In conclusion, FB-OS could reduce phosphorus concentration to less than 1 mg/L.

3.2.4 Adsorption Dynamics Fitting Results and Analysis

In order to further explore the adsorption behavior of FB-OS, the adsorption curve of FB-OS at 30°C (Fig. 5a) was fitted by pseudo-first-order (PFO) and pseudo-second-order kinetic equations (PSO), the results were shown in Table 1 and Fig. 6. It can be seen from Table 1 that PSO had the best fitting result ($R^2 = 0.995$), and its predicted saturated adsorption capacity (q_e) was 3.96 mg/g, which was close to the experimental adsorption capacity (q_{ec}) of 3.66 mg/g. In addition, PSO theory is based on divalent metal ions adsorbing polar groups (aldehydes, ketones and phenols), this is similar to Ca²⁺ adsorbing PO₄³⁻ (HPO₄²⁻ and H₂PO₄⁻) in the paper [51]. Meanwhile, according to "3.1.3" it could be seen that there were chemical reactions in the process of phosphorus removal. In summary, it was reasonable to use PSO to explain the adsorption behavior of FB-OS to phosphorus. PSO generally contains surface adsorption, outer film diffusion and intraparticle diffusion process. The surface adsorption (i.e., surface chemical reaction) rate is fast, while the outer film diffusion and intraparticle diffusion.

Table 1: Different kinetic equations fitting effects of FB-OS adsorption curve at 30°C

Kinetic equations	q _{ec} (mg/g)	q _e (mg/g)	$k_1 (h^{-1})$	$k_2 (g/(mg \cdot h))$	R^2
Pseudo-first-order rate equation	3.66	1.316	0.840	_	0.772
Pseudo-second-order rate equation	3.66	3.96	_	0.65	0.995

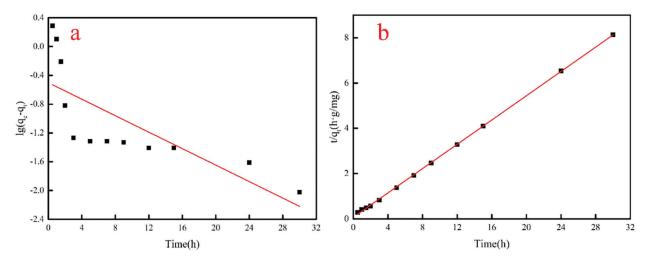


Figure 6: PFO and PSO fitting results of FB-OS at 30°C (a is the PFO fitting result, b is the PSO fitting result)

Based on the literature [50,52] and PSO model, the adsorption process can commonly be divided into three stages: rapid adsorption, slow adsorption, and equilibrium. In Fig. 5a, at 30°C, it can be seen that $0 \sim 4$ h was the rapid adsorption stage. In this process, there were a large number of PO₄³⁻ in the aqueous solution,

and FB-OS had a large number of unreacted active sites. The FB-OS was added to the phosphorus solution, and the phosphorus solution wetted the composite material and entered the interior of the composite material along the gap. And then, the rich Ca^{2+} in the FB-OS could react rapidly with PO_4^{3-} to form $Ca_3(PO_4)_2$, etc. PO_4^{3-} in phosphorus solution was quickly fixed. From 4 to 5 h, it was the slow adsorption stage. Relative to the rapid adsorption stage, during this process, phosphorus concentration in water was significantly reduced, and the concentration difference between internal and external phosphorus of FB-OS also was significantly reduced. Meanwhile, a large amount of amorphous calcium phosphate was generated on the surface and inside of FB-OS (Figs. 3d, 3e), which may be hindering the diffusion of phosphorus solution in the material. These led to a slowing down of the phosphate transfer rate inside and outside the particle. At the same time, part of active sites of FB-OS were inactivated after binding to PO_4^{3-} . Under the combined action of various factors, the adsorption rate of FB-OS decreased. In addition, a large amount of $Ca_3(PO_4)_2$ was generated at this stage, which led to the desorption rate increased. However, the adsorption rate at this stage was still greater than the desorption rate. As the adsorption proceeds, the adsorption rate gradually slowed, and the desorption rate gradually increased. When the adsorption and desorption rates were the same, FB-OS reached the adsorption equilibrium, and phosphorus was no longer adsorbed in water. This was the equilibrium stage.

4 Conclusion

Iron-pillared bentonite was prepared by modifying calcium bentonite with iron-pillared liquid, and then the composite material was prepared by mixing, granulating and calcining the iron-pillared bentonite and oyster shell powder. The characterization results showed that FB-OS generated CaO under hightemperature calcination. The maximum bending stress of FB-OS was 43.7 N, and the compressive strength was 0.927 MPa. SEM analysis showed that the structure of FB-OS was compact, but there were gaps in it. The phosphorus removal test showed that the maximum adsorption capacity of FB-OS was 48.31 mg/g, and the phosphorus removal rate was more than 90%. After phosphorus removal, SEM observed that spherical products were produced on the surface and inside FB-OS, it was speculated that they were amorphous calcium phosphate. Analysis indicated that chemical adsorption existed in the process of phosphorus removal, and the process could be expressed by PSO model: $q_t = \frac{10.193t}{1+2.574t}$ (R² = 0.995). The adsorption rate was mainly controlled by outer film diffusion and intraparticle diffusion.

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