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Investigation on the Changing Characteristics of Flow-Induced Noise in a Centrifugal Pump

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ABSTRACT

Centrifugal pumps are widely used in engineering for a variety of applications. A known drawback of these devices is the high-level noise generated during operations, which can affect their stability and adversely influence the entire working environment. By combining the Powell vortex sound theory, numerical simulations and experimental measurements, this research explores the trends of variation and the corresponding underlying mechanisms for the flow-induced noise at various locations and under different operating conditions. It is shown that the total sound source intensity (TSSI) and total sound pressure level (TSPL) in the impeller, in the region between the inlet to the outlet and along the circumferential extension of the volute, are much higher than those at pump inlet and outlet. Additionally, under various rotational speeds with the design flow rate (Condition 1), the TSSI and TSPL at pump inlet and outlet are higher than those obtained with the opening of the valve kept unchanged (Condition 2); vice versa when these two parameters are evaluated at various locations in the impeller and the volute under the Condition 2, they exceed the equivalent values obtained for the other Condition 1.

KEYWORDS

Flow-induced noise; centrifugal pump; noise evaluation criterion; Powell vortex sound theory; numerical simulations

1 Introduction

The centrifugal pumps are the main fluid transporting devices, which have played an indispensable role in many fields [1–3]. With the increasingly stringent environmental requirements, on the basis of high hydraulic performance of centrifugal pumps, the noise performance has received wide attention. Actually, the noise induced by unsteady flow in pumps has a decisive effect on whole noise level evaluation. Therefore, how to control the flow-induced noise has become an important topic for centrifugal pumps.

Currently, a number of researches have been conducted through experimental measurements and numerical simulations, to explore the generation mechanisms, distribution and propagation characteristics of flow-induced noise in centrifugal pumps. The generation of flow-induced noise was associated with various complex phenomena in pumps, including rotor-stator interaction and cavitation, etc. [3].



The rotor-stator interaction was the main cause of flow-induced noise. Generally, under the effect of rotor-stator interaction, the physical quantities (pressure, velocity, etc) in pumps showed the periodic fluctuation characteristics [4], so the flow-induced noise reached to maximum at blade-passing frequency (f_b), and also decreased with the increase of frequency [5]. The cavitation, which could affect the hydraulic performance and pump structure, was another cause of flow-induced noise [6]. With the development of cavitation, the rotor-stator interaction intensity weakened, and the noise in high frequency range increased gradually [7]. At present, the improvement of computational fluid dynamics (CFD) technology has facilitated the related researches, and the numerical model combining the CFD and Lighthill acoustic analogy theory [8,9] has been widely adopted for noise simulations. Based on the numerical model, Yang et al. [10], Si et al. [11] and Mao et al. [12] analyzed the noise directivity distribution characteristics in circumferential direction. It was revealed that the noise showed dipole symmetric distribution characteristics. Besides, the noise distribution characteristics in other directions were also revealed by Dong et al. [13] and Guo et al. [14], and the spatial directivity distribution characteristics were obtained. In addition, Guo et al. [15] conducted experiments and simulations to explore the noise propagation mechanisms from view of flow and sound fields synergy concept. The results manifested that the noise tended to propagate outside the pump with increasing the synergy degree.

The purpose of the researches on the flow-induced noise is to realize the noise control, and the passive control method [16] is the most frequently used method. Based on the passive control principle, the effect of different pump structures on the pressure fluctuation and noise has been extensively explored. Cheng et al. and Dai et al. [17,18], discussed the different structures on pressure fluctuation at various locations in pumps. Wang et al. [19] analyzed the influence of blade number on flow-induced noise at pump outlet. It was showed that the noise decreased first, then increased with the increase of blade number. Cheng et al. [20] investigated the impact of blade outlet cutting on the noise at pump inlet and outlet. The results showed that the V-shaped cutting improved the noise performance. Currently, the noise reduction researches based on bionics principle have drawn more attention. Dai et al. [21] extracted the surface features of shark and designed the V-groove surface blades for noise reduction. Zhang et al. [22] designed the orthogonal test and revealed the optimization effect of bionic blade on the noise at pump inlet and outlet. The flow-induced noise in centrifugal pumps was impacted by various structures, so the optimization of various structures was considered to reduce the noise at pump outlet. Guo et al. [23] employed the response surface method to analyze the influence of blade profile on noise at pump outlet. What's more, Si et al. [24,25], also compared the different structure combinations on the noise at pump outlet. The relevant conclusions promoted the noise optimization design of centrifugal pumps significantly.

According to the references above, the majority of researches focused on the noise distribution characteristics, while the corresponding mechanisms were rarely involved. The numerical model combining the Lighthill acoustic analogy and CFD has developed much in exploring the distribution characteristics and changing trends of noise, but the flow and sound fields are simulated separately, which is not applicable to explore the generation and changing mechanisms of flow-induced noise. Additionally, the noise optimization design was mainly realized by comparing the noise at pump outlet with different geometry parameters of pump structures, then revealing the optimal geometry parameter. However, the flow instability degree at various locations is different in pumps [17,18], the flow-induced noise at pump outlet may not be sufficient to evaluate the overall noise level in the noise optimization design process. Besides, the centrifugal pumps need to operate under various operating conditions to meet different demands, and the flow-induced noise changes accordingly. The flow-induced noise at various locations in pumps may have different changing trends with the change of operating condition, and the changing trends of noise at pump outlet with operating condition cannot be enough to reflect the overall noise accurately, which also limits the development of noise prediction research. Therefore, it is necessary to develop new numerical model to compare the flow-induced noise at various locations

and explore the changing mechanisms under various operating conditions, then propose a more suitable noise evaluation criterion.

Compared with Lighthill acoustic analogy theory, Powell vortex sound theory takes great advantages in exploring the generation and changing mechanisms of flow-induced noise [15,26]. Therefore, the numerical model combining the Powell vortex sound theory and CFD is established, and the corresponding experimental measurements are conducted to verify the accuracy of the model. Based on the numerical model and experiments, the flow-induced noise at different locations in the pump is compared under various operating conditions, and the corresponding changing mechanisms are also revealed. Then, a more suitable noise evaluation criterion is presented. The research can be used to guide the researches on the establishment of noise prediction model and the noise optimization design of centrifugal pumps.

2 Research Methodology

2.1 Physical Model

The design parameters of the model pump are listed in Tab. 1. Fig. 1 presents the 3D geometric model, which includes inlet, impeller, volute and outlet. A mesh system with tetrahedral element is generated. Tab. 2 shows the sensitivity analysis results of mesh system. It can be found that the pump head grows with the increase of mesh number. When the mesh number increases from 1.5 to 2.1 million, the growth rate of pump head is relatively large, while the pump head has little growth with the mesh number increasing from 2.1 to 2.4 million. To improve the accuracy while reducing the computational costs, Mesh-C is chosen, as shown in Fig. 2.

Table 1: Design parameters of the pump

Design parameter	Value
Design rotational speed/ $\text{r}\cdot\text{min}^{-1}$	2900
Design flow rate/ $\text{m}^3\cdot\text{h}$	50
Design head/m	80
Impeller inlet diameter/mm	80
Impeller outlet diameter/mm	250
Volute outlet diameter/mm	50
Number of blades	6

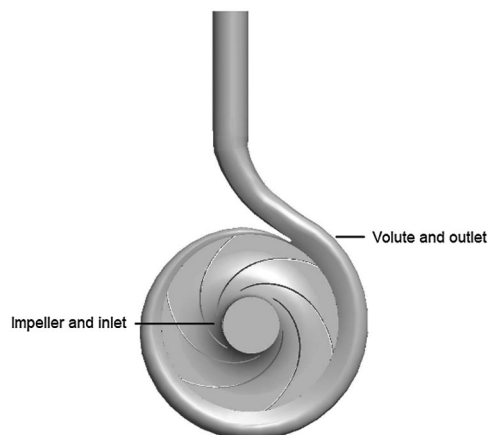
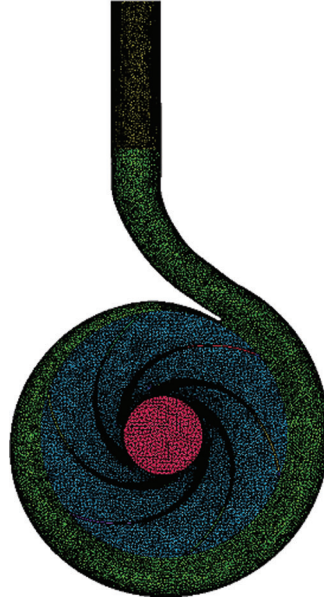


Figure 1: Geometric model

Table 2: Mesh sensitivity analysis

Mesh system	Mesh number/*10 ⁶	Pump head/m	Growth rate
Mesh-A	1.5	84.25	–
Mesh-B	1.8	84.33	0.09%
Mesh-C	2.1	84.40	0.08%
Mesh-D	2.4	84.42	0.02%

**Figure 2:** Mesh system

2.2 Mathematical Model

Water is used as the medium, which means that the flow field can be regarded as incompressible. The continuity and momentum equations of flow field are expressed as,

$$\nabla \cdot \vec{u} = 0 \quad (1)$$

$$\frac{\partial \vec{u}}{\partial t} + (\vec{u} \cdot \nabla) \vec{u} = \vec{f} - \frac{1}{\rho} \nabla p + \nu \nabla^2 \vec{u} \quad (2)$$

where \vec{u} and \vec{f} are the velocity and volume force vectors, ρ , p and ν are the density, pressure and kinematic viscosity. The Eqs. (1) and (2) are solved by using the Reynolds-averaged method. Reynolds-averaged governing equations are defined as,

$$\frac{\partial \bar{u}_i}{\partial x_i} = 0 \quad (3)$$

$$\frac{\partial \bar{u}_i}{\partial t} + \bar{u}_j \frac{\partial \bar{u}_i}{\partial x_j} = \bar{f}_i - \frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} + \frac{1}{\rho} \frac{\partial}{\partial x_j} \left(\mu \frac{\partial \bar{u}_i}{\partial x_j} - \overline{\rho u_j u_i} \right) \quad (4)$$

where the superscript “-” represents the averaged value. To solve the Eqs. (3) and (4), the standard k- ϵ model is adopted. The k and ϵ can be obtained by the following equations:

$$\frac{\partial}{\partial t}(\rho k) + \frac{\partial}{\partial x_i}(\rho k u_i) = \frac{\partial}{\partial x_i}((\mu + \frac{\mu_t}{\sigma_k}) \frac{\partial k}{\partial x_i}) + G_k + G_b - \rho \varepsilon \quad (5)$$

$$\frac{\partial}{\partial t}(\rho \varepsilon) + \frac{\partial}{\partial x_i}(\rho \varepsilon u_i) = \frac{\partial}{\partial x_i}((\mu + \frac{\mu_t}{\sigma_\varepsilon}) \frac{\partial \varepsilon}{\partial x_i}) + C_{1\varepsilon} \frac{\varepsilon}{k} (G_k + C_{3\varepsilon} G_b) - C_{2\varepsilon} \rho \frac{\varepsilon^2}{k} \quad (6)$$

Here, G_k and G_b represent the generation of turbulent kinetic energy. $C_{1\varepsilon}$, $C_{2\varepsilon}$, and $C_{3\varepsilon}$ are 1.44, 1.92 and 0.09, respectively, while σ_k and σ_ε are 1.0 and 1.3, respectively.

The contribution of viscosity to noise is small, without considering the effect of fluid viscosity, the Powell vortex sound equation is adopted for the sound field simulation, which is defined as,

$$\nabla^2 p' - \frac{1}{c_0^2} \frac{\partial^2 p'}{\partial t^2} = -\nabla \cdot (\rho(\vec{\omega} \times \vec{u})) + \nabla(\rho \frac{u^2}{2}) \quad (7)$$

where t' is the time of sound field. The equation includes spatial, time and sound source items. p' is the sound pressure, c_0 is the sound speed, $\vec{\omega}$ represents the vorticity vector.

2.3 Numerical Method

The steady and unsteady flow field simulations, as well as the unsteady sound field simulation are conducted by using Fluent. The main numerical methods used for simulation are listed in [Tabs. 3 and 4](#).

Table 3: The main numerical methods used for flow field simulation

Items	Setting
Solver	Pressure-based type
Discretization principle	Cell-centered finite volume method
Inlet	Velocity inlet
Outlet	Outflow
Wall	No slip boundary condition
Pressure-velocity coupling algorithm	Semi-implicit method for pressure linked equations algorithm [27,28]
Time step of unsteady flow field	The rotational angle changes 2° per time step
Simulation time of unsteady flow field	7–10 times of rotational period

Table 4: The main numerical methods used for sound field simulation

Items	Setting
Discretization principle	Cell-centered finite volume method
Time-matching method between flow and sound fields	Asynchronous time marching method
Solving method	Implicit iteration method
Inlet and outlet	Absorption boundary
Wall	Total reflection boundary
Initial values	0
Time step of unsteady sound field	$1.44 * 10^{-7}$ s
Simulation time of unsteady sound field	1–2 times of rotational period

The absorption boundary and total reflection boundary conditions are defined as,

$$\frac{1}{c_0} \frac{\partial p'}{\partial t} + \nabla p' \cdot \vec{n} = 0 \quad (8)$$

$$p' = 0 \quad (9)$$

where n' is the unit normal vector of boundary surface. In order to compare the flow-induced noise at various locations in impeller and volute, 10 monitoring points are arranged. As shown in Fig. 3, I1–I5 are set from inlet to outlet in the impeller, and V1–V5 are arranged along the circumferential extension of the volute. The operating conditions include various rotational speeds with design flow rate (Condition 1) and various rotational speeds with the opening of the valve kept unchanged (Condition 2). The detailed operating parameters are listed in Tabs. 5 and 6.

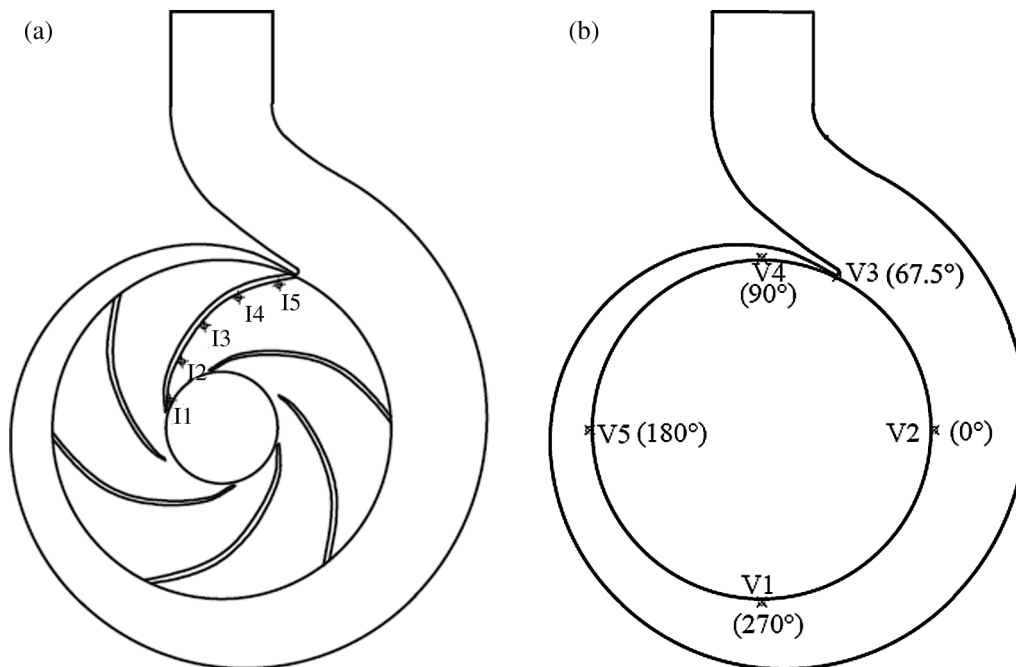


Figure 3: Monitoring arrangement (a) Monitoring points in the impeller (b) Monitoring points in the volute

Table 5: Various rotational speeds with design flow rate (Condition 1)

Rotational speed/r·min ⁻¹	Flow rate/m ³ ·h ⁻¹
2100	50
2300	50
2500	50
2700	50
2900	50

Table 6: Various rotational speeds with the opening of the valve kept unchanged (Condition 2)

Rotational speed/r·min ⁻¹	Flow rate/m ³ ·h ⁻¹
2100	36.2
2300	39.7
2500	43.1
2700	46.6
2900	50

The total sound pressure level (TSPL) and total sound source intensity (TSSI) are calculated to present the noise level and noise source level at different monitoring points. Here, TSPL and TSSI are defined as,

$$TSPL = 10 \lg \sum_{l=1}^{nm} 10^{SPL_l/10} \quad (10)$$

$$TSSI = 10 \lg \sum_{l=1}^{nm} 10^{SSI_l/10} \quad (11)$$

where nm represents the number of frequencies, while the SPL and SSI are the sound pressure level and sound source intensity at different frequencies. Besides, the averaged-total sound pressure level (L_p) and averaged-total sound source intensity (L_s) are calculated to characterize the overall noise level and noise source level of various monitoring points or different operating conditions. The L_p and L_s are defined as,

$$L_p = 10 \lg \left(\frac{1}{m} \sum_{l=1}^m 10^{TSPL_l/10} \right) \quad (12)$$

$$L_s = 10 \lg \left(\frac{1}{m} \sum_{l=1}^m 10^{TSSI_l/10} \right) \quad (13)$$

where m is the number of monitoring points or operating conditions (m = 10 or 5).

3 Experimental Validation

3.1 Experimental Setup

Owing to the difficulty of flow-induced noise measurement in impeller and volute, the noise at pump inlet and outlet is measured. The experimental setup is shown in Fig. 4. To reduce the influence of environmental noise, the measurement is conducted in a semi-anechoic chamber. The DHP8501 type hydrophone is used to measure the noise, which has the advantages of high sensitivity and wide measuring range. The rotational speed of the pump is regulated by a YVF2180L-2 type motor mounted outside the chamber, and the flow rate is controlled by a SLDG-800 type flow valve installed near the water tank.

3.2 Model Validation

The flow-induced noise at pump outlet is analyzed to validate the feasibility of the numerical model. Tab. 7 shows the comparison of f_b and corresponding SPL obtained by simulation and experiment under Condition 1. Due to the complexity and instability of the real flow in the pump, as well as the effects of environmental noise and simulation assumptions, the simulation results of flow-induced noise cannot be

completely same as the experimental results, and the deviation widely exists. It can be found that the relative errors of f_b and SPL obtained by simulation and experiment are small, and the maximum errors are -1.6% and 6.9% , respectively. In addition, the noise is the superposition result of SPL at different frequencies, thus the TSPL is also compared. As shown in Tab. 8, the TSPL at pump outlet obtained by simulation and experiment shows the similar increasing trends with the growth of rotational speed, and the maximum relative error is 1.9% . The comparison results in Tabs. 7 and 8 can validate the accuracy of the numerical model.

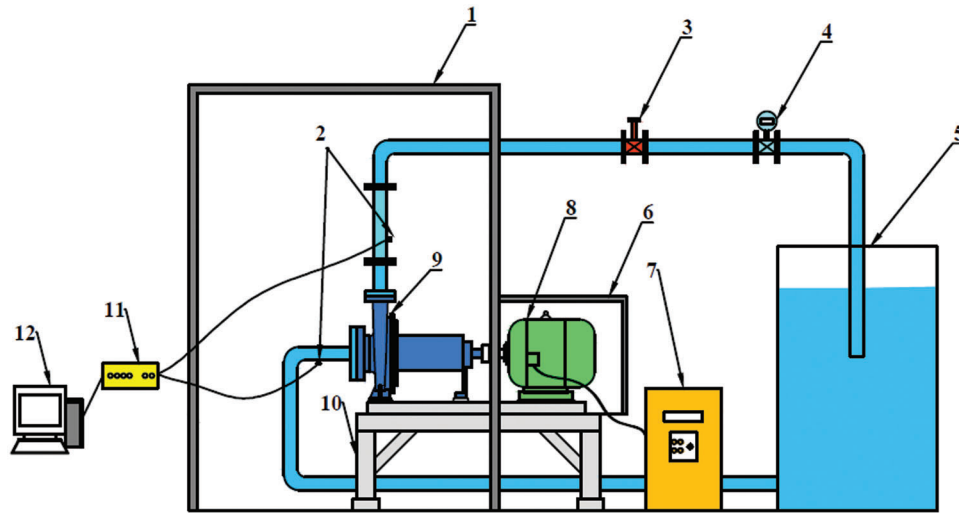


Figure 4: Experimental setup 1: Semi-anechoic chamber; 2: Monitoring points at inlet and outlet; 3: Valve; 4: Flow meter; 5: Water tank; 6: Acoustic enclosure; 7: Frequency converter; 8: Motor; 9: Pump; 10: Bracket; 11: USB switch; 12: Computer

Table 7: Comparison of SPL at f_b under Condition 1

Rotational speed/ $\text{r}\cdot\text{min}^{-1}$	f_b/Hz			SPL/dB		
	Simulation	Experiment	Relative error	Simulation	Experiment	Relative error
2100	210	213.5	-1.6%	142.7	150.6	-5.2%
2300	230	233.6	-1.5%	149	151.2	-1.5%
2500	250	253.7	-1.5%	160.4	150	6.9%
2700	270	273.8	-1.4%	158.1	151.5	4.4%
2900	290	293.9	-1.3%	156.3	152	2.8%

Table 8: Comparison of TSPL under Condition 1

Rotational speed/ $\text{r}\cdot\text{min}^{-1}$	TSPL/dB		
	Simulation	Experiment	Relative error
2100	171.2	169.2	1.2%
2300	173.5	170.2	1.9%
2500	174.5	172.1	1.4%
2700	175.8	173.2	1.5%
2900	181.8	180.6	0.7%

4 Results

4.1 Noise Comparison at Pump Inlet and Outlet

Fig. 5 shows the changing trends of TSPL at pump inlet and outlet obtained by experiment under various operating conditions. It can be found that the TSPL increases with the growth of rotational speed, and the TSPL at outlet is higher than that at inlet. When the rotational speed grows from 2100 to 2900 r/min, the TSPL at inlet and outlet increases by 1.8% and 6.5% under Condition 1, while it at inlet and outlet under Condition 2 increases by 2% and 6.9%, respectively. Besides, the TSPL at inlet and outlet under Condition 1 is 0.4% and 0.1% higher than that at inlet and outlet under Condition 2, respectively.

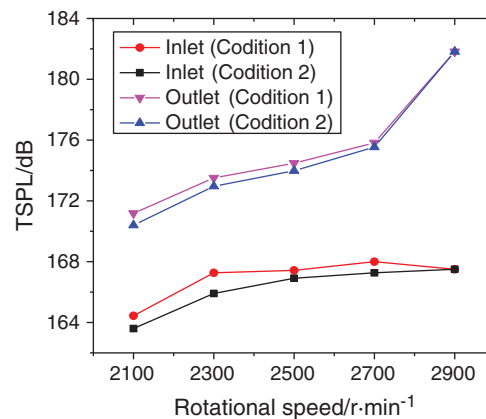


Figure 5: Changing trends of TSPL at inlet and outlet under various operating conditions

To explore the changing mechanisms of TSPL, the changing trends of TSSI with operation condition are analyzed. As shown in Fig. 6, the TSSI at outlet is higher than that at inlet, and the changing trends of TSSI with operation condition are similar to those of TSPL. When the rotational speed grows from 2100 to 2900 r/min, the TSSI at inlet and outlet increases by 2.2% and 2.9% under Condition 1, while it at inlet and outlet under Condition 2 increases by 2.6% and 4.3%, respectively. Besides, the TSSI at inlet and outlet under Condition 1 is 0.3% and 0.6% higher than that at inlet and outlet under Condition 2, respectively.

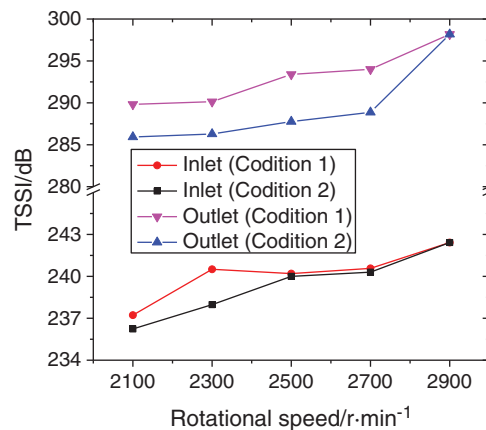


Figure 6: Changing trends of TSSI at inlet and outlet under various operating conditions

By comparing Figs. 5 and 6, it can be concluded that with the growth of rotational speed, the flow instability degree at pump inlet and outlet intensifies, which is reflected by the increase of TSSI, and the TSPL increases accordingly. Furthermore, the TSSI under Condition 1 is higher than that under Condition 2, resulting in the same changing characteristics of TSPL.

4.2 Noise Comparison at Various Locations in Impeller and Volute

Take the 2100 and 2700 r/min conditions as example, Fig. 7 shows the comparison of TSSI and TSPL at various locations in the impeller. It can be found that the TSSI increases from inlet to outlet in the impeller, which causes the similar increasing trends of TSPL, and the two parameters at different monitoring points are higher than those at inlet and outlet of the pump. Additionally, different with the changing trends of TSSI and TSPL at pump inlet and outlet, the two parameters under Condition 2 are higher than those under Condition 1 in the impeller. Specifically, the TSSI and TSPL of the monitoring points under Condition 2 are 0.2% and 0.8% higher than those under Condition 1 at 2700 r/min, while at 2100 r/min, the growing rate are 0.3% and 1.7%, respectively.

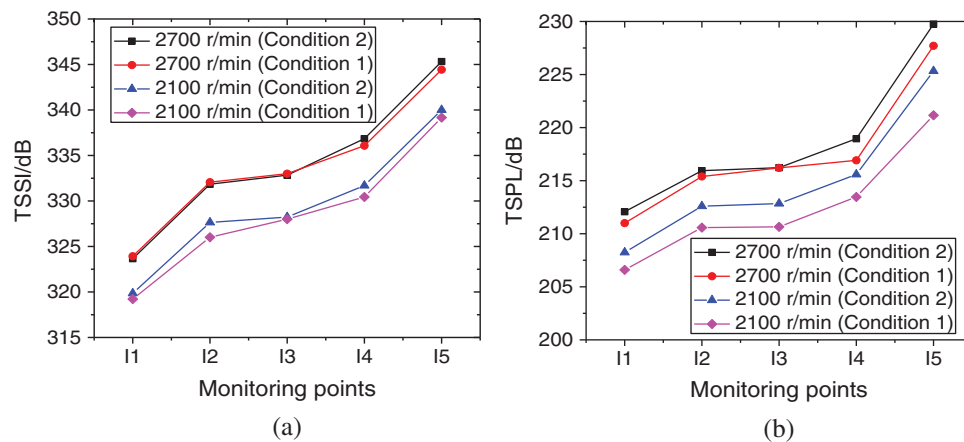


Figure 7: Changing trends of TSSI and TSPL at various locations in the impeller (a) TSSI (b) TSPL

Fig. 8 depicts the TSSI and TSPL distribution characteristics in the volute at 2100 and 2700 r/min conditions. It is revealed that the TSSI and TSPL in the volute are close to those in the impeller, and also higher than those at inlet and outlet. Similar to the changing trends of TSSI and TSPL in the impeller, the two parameters in the volute under Condition 2 are higher than those under Condition 1. More concretely, when the rotational speed is 2700 r/min, the TSSI and TSPL of the monitoring points under Condition 2 are 0.4% and 0.2% higher than those under Condition 1, while at 2100 r/min, the growing rate are 0.9% and 2.3%, respectively.

Fig. 9 illustrates the changing trends of L_s and L_p of the monitoring points in impeller and volute under various operating conditions. It can be observed that the L_s and L_p increase with the growth of rotational speed, and the two parameters under Condition 2 are 0.3% and 0.6% higher than those under Condition 1. Besides, under the same rotational speed, the lower the flow rate is, the higher the L_s representing flow instability degree in impeller and volute is, thus the L_p increases.

By comparing the Figs. 5–9, it can be revealed that the changing trends of the sound source intensity at pump inlet and outlet are different with those in impeller and volute, further causing the different changing trends of noise. Therefore, it is not suitable for the noise at pump inlet and outlet to evaluate the overall noise level in the pump. The flow-induced noise in centrifugal pumps should be evaluated by the superposition result of noise at various locations in impeller from inlet to outlet and along the circumferential extension of volute.

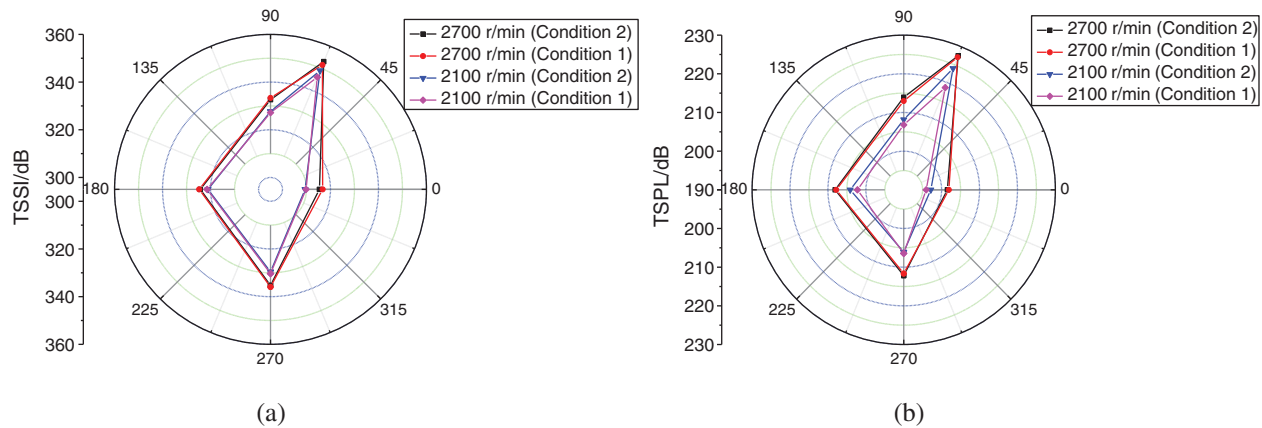


Figure 8: Distribution characteristics of TSSI and TSPL in the volute (a) TSSI (b) TSPL

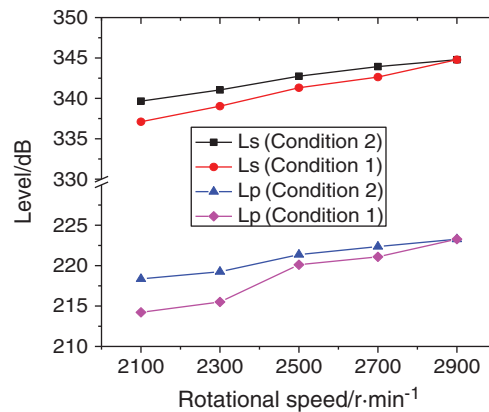


Figure 9: Changing trends of L_p and L_s under various operating conditions

5 Discussion

The accurate noise evaluation is an important basis for noise optimization of centrifugal pumps. During the noise optimization process, the previous researches mainly aimed at reducing the flow-induced noise at pump outlet. By comparing the changing trends of flow-induced noise at various locations with the change of operating condition, this research proposes that the noise evaluation should consider the comprehensive result of noise at various locations in impeller from inlet to outlet and along the circumferential extension of volute.

According to the Powell vortex sound theory, the generation of flow-induced noise is associated with the unsteady fluid flow, and the flow instability degree reflected by sound source intensity is the decisive factor on noise level. The research results imply that the flow in impeller and volute is the most unstable under the effect of impeller rotation, following by outlet pipe, and the flow in inlet pipe is relative stable, consequently, the noise at outlet is higher than that at inlet, but lower than that in impeller and volute. Furthermore, under the same rotational speed, with the decrease of flow rate, the flow at pump inlet and outlet becomes stable, while that in impeller and volute tends to be unstable, which is demonstrated by the changing trends of sound source intensity, so the noise at pump inlet and outlet, as well as that in impeller and volute show opposite changing trends. In summary, the flow-induced noise in impeller and volute should be used for noise evaluation of centrifugal pumps, which is beneficial to the noise optimization and noise prediction accurately.

Although there are important discoveries revealed by this research, the limitation also exists. The detailed monitoring points used for noise evaluation are not discussed. In the following research, we will further

compare the changing trends of noise at various locations with the change of operating condition and pump structure, then propose the representative monitoring points and corresponding noise evaluation formula.

6 Conclusions

To reveal the deficiency of current noise evaluation method, and figure out a more suitable noise evaluation criterion for noise optimization of centrifugal pumps, based on the Powell vortex sound theory, numerical simulations and experimental measurements, the flow-induced noise at various locations in a centrifugal pump is compared under various operating conditions. The conclusions are as follows:

(1) The flow instability degree at pump outlet is more intense than that at inlet, which is characterized by the TSSI at outlet being higher than that at inlet, consequently, the TSPL at outlet is higher than that at inlet under different operating conditions. In addition, under the same rotational speed, the TSSI under large flow rate condition is higher than that under small flow rate condition, which further causes the similar distribution characteristics of TSPL. Specifically, the TSSI and TSPL at pump inlet and outlet under Condition 1 are 0.3% and 0.6%, 0.4% and 0.1% higher than those under Condition 2, respectively.

(2) Compared with the TSSI at pump inlet and outlet, the TSSI at various locations in impeller from inlet to outlet and along the circumferential extension of volute is much higher, which means that the flow in impeller and volute is more unstable, and further induces high-level noise. Besides, under the same rotational speed, the TSSI and TSPL at various locations under small flow rate condition is higher than that under large flow rate condition. The L_s and L_p of various monitoring points in impeller and volute under Condition 2 are 0.3% and 0.6% higher than those under Condition 1, which are opposite with the changing trends of those at pump inlet and outlet of the pump.

Briefly, the changing trends of flow-induced noise at pump inlet and outlet are different with those in impeller and volute, and the noise in impeller and volute is much higher than that at pump inlet and outlet. Therefore, the superposition result of noise at various locations in impeller from inlet to outlet and along the circumferential extension of volute should be considered to evaluate the flow-induced noise in centrifugal pumps.

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