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# Numerical Simulation for Bioconvection of Unsteady Stagnation Point Flow of Oldroyd-B Nanofluid with Activation Energy and Temperature-Based Thermal Conductivity Past a Stretching Disk

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## ABSTRACT

A mathematical modeling is explored to scrutinize the unsteady stagnation point flow of Oldroyd-B nanofluid under the thermal conductivity and solutal diffusivity with bioconvection mechanism. Impacts of Joule heating and Arrhenius activation energy including convective boundary conditions are studied, and the specified surface temperature and constant temperature of wall (CTW) are discussed. The consequences of thermal conductivity and diffusivity are also taken into account. The flow is generated through stretchable disk geometry, and the behavior of non-linear thermal radiation is incorporated in energy equation. The partial differential equations governing the fluid flow in the structure is reduced into dimensionless nonlinear ODEs by applying suitable similarity variables. The obtained system of non-dimensional nonlinear ODEs is treated numerically with the help of bvp4c solver in Matlab under shooting algorithm. The impact of various prominent parameters on velocity profile, thermal profile, volumetric nanoparticle concentration and microorganism distribution is depicted in graphical form. The numerical outcomes for skin friction coefficient, heat transfer rate, Sherwood number as well as microorganism density number versus various parameters are listed in the tables. The results show that fluid velocity is reduced by increasing buoyancy ratio parameter, while the fluid flow increases with mixed convective parameter. The temperature profile is enhanced with the amount of nonlinear thermal radiation and temperature dependent thermal conductivity. Furthermore, concentration profiles of nanoparticles have opposite behavior for Brownian motion coefficient and thermophoresis diffusion parameter, and it is noticed that by varying Peclet number the microorganisms profile is declined. The proposed study is useful to control and optimize heat transfer in industrial applications.

## **KEYWORDS**

Oldroyd-B nanofluid; thermal conductivity; solutal diffusivity conductivity; bioconvective microorganisms; shooting algorithm



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## Nomenclature

PST	Surface temperature
CWT	Constant wall temperature
$\lambda_1$	Relaxation time
р	Pressure of fluid
С	Concentration
N	Microorganisms
α	Fluid heat diffusivity
$D_B$	Brownian diffusion coefficient
$D_T$	Brownian thermophoresis coefficient
$k_1$	Chemical reaction constant
$h_T$	Heat transfer coefficient
$h_C$	Mass transfer coefficient
S	Unsteadiness parameter
M	Magnetic parameter
Nb	Brownian motion coefficient
λ	Mixed convection parameter
$Ec_r$	Eckert number
Nt	Thermophoresis diffusion parameter
Nr	Buoyancy ratio parameter
Nc	Bioconvection Rayleigh number
$K_1$	Chemical reaction parameter
Ε	Activation energy parameter
Bi	Biot number
Pe	Peclet number
Ω	Microorganism difference variable
f'	Characteristics of velocity distribution
$\theta$	Thermal profile
$\phi$	Solutal field of nanomaterials
χ	Motile microorganism's profiles
Ε	Activation energy
Pe	Peclet number
Pr	Prandtl number
$ heta_w$	Temperature ratio parameter
Rd	Radiation parameter
Le	Lewis number
Lb	Bioconvection Lewis number
S	Unsteadiness parameter
$\alpha_1$	Deborah number for relaxation to time parameter
$\alpha_2$	Deborah number for retardation to time parameter
$\varepsilon_1$	Thermal conductivity
$\varepsilon_2$	Solutal diffusivity parameter
Κ	Velocity ratio parameter
Т	Temperature
С	Concentration

## **Greek Symbols**

ρ	Density of fluid
v	Kinematic viscosity

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#### **1** Introduction

#### 1.1 Review of the Literature

Transmission of heat integrated liquid flow is necessary for a significant number of nuclear and thermal-hydraulic systems. The involvement of liquids in the these systems can help to reduce capital costs, enhance operating efficiency and improve the performance of the system. Amongst various conventional methods, air is one of the main techniques of cooling electrical devices. The cooling is necessary in order to maintain the required thermal efficiency in different scientific and technological products such as computers, engines, chemical processes, and so on. Nanofluids, due to their exceptional thermo-physical characteristics and relatively slower heat resistance, have recently obtained the most attractive interest. Nanoparticles are comparatively tiny-sized particles that are contained in the fluid. The main purpose of introducing such particles are to enhance the heat conductivity of commonly utilized base liquids. The definition of nanofluid was initiated by Choi [1] who demonstrated that a host liquid, including water or ethylene-glycol fluid, can increase its heat efficiency by incorporating nanoparticles. Later, Buongiorno [2] identified Brownian motion and thermophoresis elements for the development of nanoparticles associated with heat transport. Aminian et al. [3] studied the impacts of  $Al_2O_3$ -CuO-water-based nano liquid in a partition cylinder surrounded by a porous channel. Saha [4] evaluated the impact of the external electromagnetic field upon on free convection movement of the  $Al_2O_3$ -water nano liquid through the internal cylindrical wall. The radiation impacts under the Magnetohydrodynamic (MHD) movement of Casson-type nano liquid across a shrinking/stretched cylinder in the presence of chemical processes were reported by Bhandari et al. [5]. Mondal et al. [6] evaluated a steady 2-dimensional (MHD) Magnetohydrodynamic mixed convection flow of viscous nano liquid and heat transformation in an inclined stretched cylinder with a chemical process and a uniformly magnetic field. Basha et al. [7] discussed the properties of fluid transportation and entropy production of tangent hyperbolic nano liquid across a horizontal revolving cylinder with the impact of nonlinear Boussinesq estimation. Sheikholeslami et al. [8] studied the influence of the helical-twisting system on the thermal-hydraulic quantity of the nano liquid flow through tube. Sudarsana Reddy et al. [9] explored the thermal and solutal transformation properties of nano-liquid flow across a stretchable surface embedded in a porous medium. Mishra et al. [10] scrutinized the motion and thermal characteristics of magnetized silver-water  $(Ag/H_2O)$  nano liquid across a stretched cylinder. Zainal et al. [11] studied the occurrence of non-unique solutions in boundary layer flow owing to deformable surfaces under the implementation of specified surface heat flux. Saeed et al. [12] researched the heat properties of the Magnetohydrodynamic hybrid nano liquid  $(Al_2O_3 - Cu/H_2O)$  flowing through permeable stretched cylinder in a Darcy medium. Jabbar et al. [13] observed the thermal properties of nanofluid in rotating cylinders under convective circumstances. Goudarzi et al. [14] evaluated the influence of nanomaterials migration in terms of Brownian motion coefficient and thermophoresis coefficient on natural convection of (Ag-MgO)/hybrid-based nano liquid. The mathematical model of MHD mixed convective flow in a trapezoidal enclosure filled with a porous-saturated Cu-water nano liquid was introduced by Ali et al. [15].

Mass exchange method coupled with chemical processes through activation energy is usually important in geothermal and oil reservoirs manufacturing, chemical engineering, and water and oil emulsion system, food preparation, and so on. It is important to establish conceptual outcomes for estimating the effect of activation energy across flows. The terminology Arrhenius activation energy was initially pioneered by Svante Arrhenius scientist in 1889. It is the lowest energy needed to transform the reactants into materials. Using a numerical method, Bestman [16] studied the free

convection boundary layer flow when the boundary wall moves in its own plane via Arrhenius activation energy. Ramesh [17] studied viscoelastic nanofluid influenced by activation energy and chemical processes. Abuzaid et al. [18] investigated numerically the mixed convective movement of Oldroyd-B nano liquid subjected to Arrhenius activation energy and binary chemical processes. Waqas et al. [19] researched the nonlinear radiation flow of Eyring-Powell nano liquid with magnet dipoles and Arrhenius activation energy. The consequence of activation energy for the Carreau-Yasuda nanofluid flow was examined by Khan et al. [20].

Non-Newtonian liquids have become very unique in the manufacturing and engineering sectors. Commonly non-Newtonian fluids are divided into three categories: (I) the differential type fluids, (II) the rate type fluids, and (III) the integral type non-Newtonian fluids. Oldroyd-B fluid is an important sub-class of the rate-type fluid. Such fluids play an important role in industrial processes such as pharmaceutical industries, paper production, food processing, drug delivery, and cancer treatment. The Oldroyd-B fluid model was first introduced by Oldroyd in 1950 [21], motivated by the research of Fröhlich et al. [22] who developed a structured method for the improvement of viscoelastic fluid modeling techniques. The 2-dimensional flow of Oldroyd-B nano liquid through the nonlinearly stretchable sheet with the Cattaneo Christov heat flux model was studied by Ibrahim et al. [23]. The improvement of dual stratification in the nonlinear radiative movement of Oldroyd-B nano liquid was explained by Irfan et al. [24]. Anwar et al. [25] evaluated the consequence of Newtonian thermal conductivity by the unsteady natural convectional movement of Oldroyd-B nanofluid contained in an infinite, vertical stationary plate. Interested readers may refer to [26,27] for more works on Oldroyd-B fluid.

Bioconvection is a naturally occurring phenomenon in swimming motile microorganisms. One type of motile microorganism, identified as the gyrotactic microorganism, is highly present in the aqueous system, which can swim in the flowing liquid along a specific direction with a fragile horizontal vortex and unstably fall in the flowing liquid with a significant horizontal vortex. Gyrotactic motile microorganism swimming components are important for understanding many ecological features of bioconvection. Microorganism molecules are used for the processing of agricultural materials including ethanol, fertilizers, biofuels, water plants as well as biodiesel. Bioconvection is an unrequested modification of macroscopic liquid patterns, including diminishing plumes. Two principal forms of up-swimming micro-organisms are normally utilized in convectional experimentation: low-heavy algae and solid oxytactic organisms. The terminology bioconvection was first proposed by Platt [28] in 1961, who described the formation of cells induced by microorganisms in the aqueous suspension. Mondal et al. [29] scrutinized the behavior of bioconvective phenomenon in nano liquid. Khan et al. [30] scrutinized the properties of a magnetic modified Newtonian fluid through bioconvection and chemically reactive organisms. Several investigators researched the bioconvective phenomenon, see [31–37]. Song et al. [38] conducted the analysis of the bioconvective

phenomenon in micropolar nano liquid over the off-centered disk. The effects of exponential base heat source/sink and Cattaneo-Christov Laws on bioconvective Carreau nano liquid were analyzed by Farooq et al. [39]. Tlili et al. [40] scrutinized the use of Arrhenius energy with thermal radiative implications in the convectional flow of magnetic Oldroyd-B nanomaterials through a stretched cylinder. A mathematical method focusing on two-dimensional modified second-grade nano liquids against revolving Riga plate for the influence of the Arrhenius activation energy and bioconvection facets was examined by Wagas et al. [41].

In this work, a new class of fluid namely nanofluid is introduced, which has high thermal conductivity. Nanofluids are mostly utilized for their improved heat characteristics as a cooling medium in heat transformation equipment like radiators, cooling of microelectronics, and fuel cells. Inspired by the above studies, the main objective is to examine the impact of non-linearly thermal radiation on the stagnation point flow of bio-convective Oldroyd-B nano liquid past a stretchable disc with activation energy. The effects of temperature-based thermal efficiency and thermal diffusivity are investigated. The current model is explored for both constant wall temperature and prescribed surface temperature cases. The similarity transformations are used to obtain the ordinary differential equation from the developed system of PDEs. The numerical solution of ODEs is found by using the shooting scheme via the bvp4c MATLAB tool. The effect of flow governing parameters is illustrated for velocity profile, a thermal profile of species, concentration, and swimming microorganism field.

#### 2 Problem Modling

Consider unsteady, 2-D stagnation point fluid flow of electrical conducting Oldroyd-B nano liquid with bioconvective swimming microorganism above a linearly stretching disk. Select a polar coordinate arrangement (r, z) in which *r*-axes are taken in the horizontal directions over the stretched disk and *z*-axis is considered in the vertically upward direction respectively. The physical schematic and coordinate classification are exhibited in Fig. 1. The velocities are considered as  $u_w(t,r) = \frac{ar}{1-\gamma t}$  and  $u_e(t,r) = \frac{cr}{1-\gamma t}$ , respectively, where *a*, *c* &  $\gamma$  are positive constants and the velocity  $u_w(t,r) = \frac{ar}{1-\gamma t}$  is along the *z* direction. The plane of the disk is exposed to the convective boundary conditions. In addition, the convective heat and mass transformation mechanisms are involved in the absence of heat production. With these assumptions, the physically governing boundary layer system of continuity, velocity, energy, the concentration of nanoparticles diffusion, and microorganism distribution in the occurrence of thermal radiative and magnetic fields over stretched disk can be described as [42,43].

$$\frac{\partial(ru)}{\partial r} + \frac{\partial(rw)}{\partial z} = 0,\tag{1}$$

$$\begin{aligned} \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial r} + w \frac{\partial u}{\partial z} + \lambda_1 \left\{ \frac{\partial^2 u}{\partial t^2} + 2u \frac{\partial^2 u}{\partial t\partial r} + 2w \frac{\partial^2 u}{\partial t\partial z} + u^2 \frac{\partial^2 u}{\partial r^2} + 2uw \frac{\partial^2 u}{\partial r\partial z} + w^2 \frac{\partial^2 u}{\partial z^2} \right\} \\ &= -\frac{1}{\rho} \frac{\partial p}{\partial r} + v \left[ \frac{\partial^2 u}{\partial z^2} \right] + \lambda_2 v \left( \frac{\partial^3 u}{\partial t\partial z^2} + w \frac{\partial^3 u}{\partial z^3} + u \frac{\partial^3 u}{\partial r\partial z^2} - 2 \frac{\partial^2 u}{\partial r\partial z} \frac{\partial u}{\partial z} - 3 \frac{\partial u}{\partial r} \frac{\partial^2 u}{\partial z^2} - \frac{\partial u}{\partial z} \frac{\partial^2 w}{\partial z^2} \right) \end{aligned}$$
(2)  
$$&- \frac{\sigma \beta_0^2}{\rho} \left[ u + \lambda_1 \left\{ \frac{\partial u}{\partial t} + w \frac{\partial u}{\partial z} \right\} \right] + \frac{1}{\rho_f} \left[ \frac{(1 - C_f) \rho_f \beta^{**} g * (T - T_\infty)}{-(\rho_p - \rho_f) g^* (C - C_\infty)} \right] \\ -(N - N_\infty) g^* \gamma (\rho_m - \rho_f) \right] \end{aligned}$$
(3)  
$$&+ Q_0 \left( \frac{T - T_\infty}{(\rho c_p)_f} \right) + \frac{\sigma \beta_0^2 u^2}{(\rho c_p)_f} + \frac{16\sigma^*}{3\rho c_p k^*} \frac{\partial}{z} \left( T^3 \frac{\partial T}{\partial z} \right), \end{aligned}$$

$$\frac{\partial C}{\partial t} + u \frac{\partial C}{\partial r} + w \frac{\partial C}{\partial z} = \frac{1}{\rho c_p} \frac{\partial}{\partial z} \left[ D(C) \frac{\partial C}{\partial z} \right] + D_B \left[ \frac{\partial^2 C}{\partial z^2} \right] + \frac{D_T}{T_\infty} \left[ \frac{\partial^2 T}{\partial z^2} \right] -kr^2 (C - C_\infty) \left( \frac{T}{T_\infty} \right)^n \exp\left( \frac{-E_a}{K_1 T} \right),$$
(4)

$$\frac{\partial N}{\partial t} + u \frac{\partial N}{\partial r} + w \frac{\partial N}{\partial z} + \left[ \frac{\partial}{\partial z} \left( N \frac{\partial C}{\partial z} \right) \right] \frac{b W_c}{(C_w - C_\infty)} = D_m \frac{\partial}{\partial z} \left( \frac{\partial N}{\partial z} \right), \tag{5}$$



Figure 1: Physical layout of the flow

with the appropriate constraints:

$$u(t,r,z) = u_w(t,r) = \frac{ar}{1-\gamma t}, \quad w(t,r,z) = 0,$$

$$-k\frac{\partial T}{\partial z} = h_T(T_w - T), \quad D_B\frac{\partial C}{\partial z} + \frac{D_T}{T_\infty}\frac{\partial T}{\partial z} = 0, \quad N = N_w \text{ at } z = 0,$$

$$u = u_e = \frac{cr}{1-\gamma t}, \quad w \to 0, \quad T \to T_\infty, \quad C \to C_\infty, \quad N \to N_\infty, \text{ as } z \to \infty.$$
(6)
(6)
(7)

Here, the relaxation time is denoted by  $\lambda_1$ , p, T, C and N represent the fluid pressure, temperature, concentration, and bioconvection respectively;  $\nu$  is the kinematic viscosity,  $\alpha$  is the fluid heat diffusivity and  $\rho$  is the fluid density,  $D_B$  and  $D_T$  are the Brownian motion and thermophoretic coefficients,  $k_1$  is the chemical reaction constant, and  $h_T$  and  $h_C$  denote the heat and mass transfer coefficients.

Variable conductivities for heat and mass are given below:

$$K(T) = k_{\infty} \left[ 1 + \epsilon_1 \left( \frac{T - T_{\infty}}{\Delta T} \right) \right], D(C) = D_{\infty} \left[ 1 + \epsilon_2 \left( \frac{C - C_{\infty}}{\Delta C} \right) \right].$$

With the similarity transformations given by [44,45]

$$u = \frac{ar}{1 - \gamma t} f'(\zeta), \quad w = -2\sqrt{\frac{av}{1 - \gamma t}} f(\zeta),$$

$$T = T_{\infty} + (T_w - T_{\infty})\theta(\zeta)(CWT),$$

$$T = T_{\infty} + \frac{br}{1 - \gamma t}\theta(\zeta)(PST), \quad \phi(\zeta) = \frac{C - C_{\infty}}{C_w - C_{\infty}},$$

$$\chi(\zeta) = \frac{N - N_{\infty}}{N_w - N_{\infty}}, \quad \zeta = z\sqrt{\frac{a}{\nu(1 - \gamma t)}},$$
Eqs. (2)–(5) reduce to the following forms:  
(8)

$$\frac{S}{2}\alpha_{2}\zeta f^{iv} - \alpha_{2}ff^{iv} - \alpha_{2}f''^{2} + 2\alpha_{2}Sf''' - 2\alpha_{2}f'f''' + f''' - \frac{S}{2}\zeta f'' - Sf' - f'^{2} + 2ff'' -\frac{7}{4}\alpha_{1}S^{2}\zeta f'' - \frac{\alpha_{1}}{4}\zeta^{2}S^{2}f''' - 2\alpha_{1}S^{2}f' - 2S\alpha_{1}f'^{2} - \alpha_{1}\zeta Sf'f'' + 2S\alpha_{1}\zeta ff''' + 6S\alpha_{1}ff'' +4\alpha_{1}ff'f'' - 4\alpha_{1}f^{2}f''' - M\left(f' + \alpha_{1}\frac{S}{2}\eta f'' + \alpha_{1}Sf' - 2\alpha_{1}ff'' - K - \alpha_{1}KS\right) + KS +K^{2} + \alpha_{1}(2KS^{2} + 2K^{2}S) + \lambda(\theta - Nr\phi - Nc\chi) = 0,$$
(9)

$$(1 + \epsilon_{1}\theta)\theta'' + \epsilon_{1}\theta'^{2} + \frac{4}{3}Rd \begin{bmatrix} \theta'' + (\theta_{w} - 1)^{3}(3\theta^{2}\theta'^{2} + \theta^{3}\theta'') \\ + 3(\theta_{w} - 1)^{2}(2\theta\theta'^{2} + \theta^{2}\theta'') \\ + 3(\theta_{w} - 1)(\theta'^{2} + \theta\theta'') \end{bmatrix} + \Pr\left(2f\theta' - \frac{S}{2}\zeta\theta'\right)$$
(10)

+ 
$$\Pr Nb\theta'\phi'$$
 +  $\Pr Nt{\theta'}^2$  +  $\Pr MEc_r {f'}^2$  +  $\Pr \delta\theta = 0$ , (*CWT*)

$$(1 + \epsilon_{1}\theta)\theta'' + \epsilon_{1}\theta'^{2} + \frac{4}{3}Rd \begin{bmatrix} \theta'' + (\theta_{w} - 1)^{3}(3\theta^{2}\theta'^{2} + \theta^{3}\theta'') \\ + 3(\theta_{w} - 1)^{2}(2\theta\theta'^{2} + \theta^{2}\theta'') \\ + 3(\theta_{w} - 1)(\theta'^{2} + \theta\theta'') \end{bmatrix} + \Pr\left(2f\theta' - S\theta - \theta f' - \frac{S}{2}\zeta\theta'\right)$$
(11)

+ 
$$\Pr Nb\theta'\phi'$$
 +  $\Pr Nt{\theta'}^2$  +  $\Pr MEc_r f'^2$  +  $\Pr \delta\theta = 0$ , (*PST*)

$$(1 + \epsilon_2)\phi'' + \epsilon_2 {\phi'}^2 + Le \Pr\left(2f\phi' - \frac{S}{2}\zeta\phi'\right) + Le \Pr\frac{Nt}{Nb}\theta'' - Le \Pr\sigma(1 + \delta\theta)^n \exp\left(\frac{-E}{1 + \delta\theta}\right)\phi = 0,$$
(12)

$$\chi'' + Lb\left(2f\chi' - \frac{S}{2}\zeta\chi'\right) - Pe[\chi'\phi' + (\Omega + \chi)\phi''] = 0,$$
(13)

with

$$f(0) = 0, \quad f'(0) = 1, \quad \theta'(0) = -Bi(1 - \theta(0)),$$
  

$$\phi'(0) + \frac{Nt}{Nb}\theta'(0) = 0, \quad \chi(0) = 1,$$
(14)

$$f'(\infty) = K, \quad \theta(\infty) = 0, \quad \phi(\infty) = 0, \quad \chi(\infty) = 0.$$
(15)

In the above equations,  $S = \frac{\gamma}{a}$  represents the unsteadiness parameter,  $\alpha_1 = \frac{\lambda_1 a}{1 - \gamma t}$  is the Deborah number of relaxation time,  $\alpha_2 = \frac{a\lambda_2}{1 - \gamma t}$  is the Deborah number of retardation time.  $K = \frac{c}{a}$  is the velocity ratio parameter,  $M = \frac{\sigma B_0^2 (1 - \gamma t)}{(\rho_f) a}$  denotes the magnetic parameter,  $Nb = \frac{\tau D_B(\Delta C)}{\nu}$  is the Brownian motion parameter,  $Ec_r = \frac{u_w^2}{c_p \Delta T (1 - \gamma t)}$  is the Eckert number,  $\lambda = \frac{\beta^{**}g * (1 - C_\infty)(T_w - T_\infty)}{a(1 - \gamma t)}$  represents the Mixed convection parameter,  $Nt = \frac{\tau D_T(\Delta T)}{\nu T_\infty}$  stands for thermophoresis parameter,  $Nr = \frac{(\rho_p - \rho_f)(C_w - C_\infty)}{\rho_f(1 - C_\infty)(T_w - T_\infty)\beta^{**}}$  is the Buoyancy ratio parameter, and  $Nc = \frac{\gamma * (\rho_m - \rho_f)(N_w - N_\infty)}{\rho_f(1 - C_\infty)(T_w - T_\infty)\beta^{**}}$  is the Bioconvectional Rayleigh number. Prandtl number is symbolized by  $Pr = \frac{v}{\alpha_1}$ ,  $\delta = \frac{Q_0(1 - \gamma t)}{a(\rho c_p)}$  is the heat source/sink parameter,  $K_1 = \frac{k_1(1 - \gamma t)}{a}$ represents the chemical reaction,  $E = \frac{E_a}{K_1 T_{\infty}}$  stands for the activation energy,  $Le = \frac{\alpha_1}{D_B}$  is the Lewis number,  $Bi = \frac{h_T}{k} \sqrt{\frac{v(1 - \gamma t)}{a}}$  is the Biot number, the bioconvection Lewis number is symbolized by  $Lb = \frac{v}{D_m}$ , the Peclet number is denoted as  $Pe = \frac{bW_c}{D_m}$ , and the microorganisms difference variable is represented by  $\Omega = \frac{N_{\infty}}{N_w - N_{\infty}}$ .

The engineering quantities of interest include:

$$C_{f} = \frac{\sqrt{\tau_{zr}^{2} + \tau_{z\varphi}^{2}}}{\rho(ar)^{2}}, \quad Nu_{r} = \frac{r}{(T_{w} - T_{\infty})} \left( 1 + \frac{16\sigma^{*}T^{3}}{3\rho c_{p}k^{*}} \right) \left( \frac{\partial T}{\partial z} \right) \Big|_{z=0}$$

$$Sh_{r} = -\frac{r}{(C_{w} - C_{\infty})} \left( \frac{\partial C}{\partial z} \right) \Big|_{z=0}, \quad Sn_{r} = -\frac{r}{(N_{w} - N_{\infty})} \left( \frac{\partial N}{\partial z} \right) \Big|_{z=0}$$

$$(16)$$

By adopting similarity transformations, the dimensionless form of engineering quantities are:

$$C_{f} \operatorname{Re}_{r}^{0.5} = \sqrt{f''^{2}(0)},$$

$$Re^{-0.5} Nu_{r} = -\left(1 + \frac{4}{3}(1 + (\theta_{w} - 1)\theta(0))^{3}\right)\theta'(0),$$

$$\operatorname{Re}^{-0.5} Sh_{r} = -\phi'(0),$$

$$\operatorname{Re}^{-0.5} Sn_{r} = -\chi'(0).$$
(17)

#### **3** Numerical Algorithm

In this section, the obtained dimensionless nonlinear (ODEs) (9)–(13) subject to the boundary constraints (14), (15) are numerically integrated by applying bvp4c solver in MATLAB software. The shooting method is utilized to transform the higher-order non-dimensional flow system into the first ordered boundary value problem. For this purpose, we introduce some new variables such as:

Let us suppose that the transformed variables as

$$f = y_{1}, \quad f_{\zeta} = y_{2}, \quad f_{\zeta\zeta} = y_{3}, \quad f_{\zeta\zeta\zeta} = y_{4}, \quad f_{\zeta\zeta\zeta\zeta} = y'_{4}$$
  

$$\theta = y_{5}, \quad \theta_{\zeta} = y_{6}, \quad \theta_{\zeta\zeta} = y'_{6}$$
  

$$\phi = y_{7}, \quad \phi_{\zeta} = y_{8}, \quad \phi_{\zeta\zeta} = y'_{8},$$
  

$$\chi = y_{9}, \quad \chi_{\zeta} = y_{10}, \quad \chi_{\zeta\zeta} = y'_{10},$$
  
(18)

$$y_{4}' = \frac{\begin{bmatrix} -y_{4} - 2S\alpha_{1}\zeta y_{1}y_{4} + \frac{\alpha_{1}}{4}\zeta^{2}S^{2}y_{4} + 4\alpha_{1}y_{1}^{2}y_{4}\frac{S}{2}\zeta y_{3} + Sy_{2} + y_{2}^{2} - 2y_{1}y_{3} \\ + \frac{7}{4}\alpha_{1}S^{2}\zeta y_{3} + 2\alpha_{1}S^{2}y_{2} + 2S\alpha_{1}y_{2}^{2} + \alpha_{1}\zeta Sy_{2}y_{3} - 6S\alpha_{1}y_{1}y_{3} - 4\alpha_{1}y_{1}y_{2}y_{3} \\ + M\left(y_{2} + \alpha_{1}\frac{S}{2}\zeta y_{3} + \alpha_{1}Sy_{2} - 2\alpha_{1}y_{1}y_{3} - K - \alpha_{1}KS\right) - KS - K^{2} - \alpha_{1}\left(\frac{2KS^{2}}{+2K^{2}S}\right) \\ - \alpha_{2}y_{3}^{2} - 2\alpha_{2}Sy_{4} + 2\alpha_{2}y_{2}y_{4}y_{2}y_{3} - \lambda(y_{4} - Nry_{6} - Ncy_{8}) \\ \hline \left[\frac{S}{2}\alpha_{2}\zeta - \alpha_{2}y_{1}\right], \qquad (19)$$

$$y_{6}^{\prime} = \frac{-\epsilon_{1}y_{6}^{2} - \frac{4}{3}Rd\left[(\theta_{w} - 1)^{3}(3y_{5}^{2}y_{6}^{2}) + 3(\theta_{w} - 1)^{2}(2y_{5}y_{6}^{2}) + 3(\theta_{w} - 1)y_{6}^{2}\right]}{(1 + \epsilon_{1}) + \frac{4}{3}Rd(1 + (\theta_{w} - 1)^{3}y_{5}^{3}) + 3(\theta_{w} - 1)^{2}y_{5}^{2} + 3(\theta_{w} - 1)y_{5})}, (CWT)$$

$$(20)$$

$$y_{6}^{\prime} = \frac{-\epsilon_{1}y_{6}^{2} - \frac{4}{3}Rd[(\theta_{w} - 1)^{3}(3y_{5}^{2}y_{6}^{2}) + 3(\theta_{w} - 1)^{2}(2y_{5}y_{6}^{2}) + 3(\theta_{w} - 1)y_{6}^{2}]}{-\Pr\left(2y_{1}y_{6} - Sy_{5} - y_{5}y_{2} - \frac{S}{2}\zeta y_{6}\right) - \Pr Nby_{6}y_{8} - \Pr Nty_{6}^{2} - \Pr MEc_{r}y_{2}^{2}}{\frac{-\Pr \delta y_{5}}{(1 + \epsilon_{1}) + \frac{4}{3}Rd(1 + (\theta_{w} - 1)^{3}y_{5}^{3}) + 3(\theta_{w} - 1)^{2}y_{5}^{2} + 3(\theta_{w} - 1)y_{5})}}, (PST)$$

$$(21)$$

$$y_{8}' = \frac{-\epsilon_{2}y_{8}^{2} - Le \Pr\left(2y_{1}y_{8} - \frac{S}{2}\zeta y_{8}\right) - Le \Pr\frac{Nt}{Nb}y_{6}'}{(1 + \delta y_{5})^{n} \exp\left(\frac{-E}{1 + \delta y_{5}}\right)y_{7}},$$
(22)

$$y_{10}' = -Lb\left(2y_1y_{10} - \frac{S}{2}\zeta y_{10}\right) + Pe[y_{10}y_8 + (\Omega + y_9)y_8'],$$
(23)

$$y_1(0) = 0, \quad y_2(0) = 1, \quad y_6(0) = -Bi(1 - y_5(0)),$$
  

$$y_8(0) + \frac{Nt}{Nb}y_6(0) = 0, \quad y_9(0) = 1,$$
(24)

$$y_2(\infty) = K, \quad y_5(\infty) = 0, \quad y_7(\infty) = 0, \quad y_9(\infty) = 0.$$
 (25)

#### **4** Result and Discussion

The unsteady natural convection of Oldroyd-B nano liquid via stretchable disk has been investigated. The numerical solution is obtained by utilizing MATLAB inbuilt function bvp4c, and the physical characteristics of the nanofluid is described by Buongiorno model. This section scrutinizes the influence of important physical parameters on quantities of substantial concentration. As sketched in Fig. 1, our aim is to visualize the characteristics of velocity distribution f', thermal profiles  $\theta$ , solutal field of nanomaterials  $\phi$ , and motile microorganism profiles  $\chi$  against an involved physical parameter such as the Brownian diffusion coefficient Nb, the thermophoretic diffusion coefficient Nt, the activation energy E, the Peclet number Pe, the Mixed convection parameter  $\lambda$ , the Prandtl number Pr, the temperature ratio parameter  $\theta_w$ , the Radiation parameter Rd, the Lewis number Le, the velocity ratio parameter K, the Lewis number Lb, the magnetic parameter M, the Buoyancy ratio parameter Nr, the Bioconvectional Rayleigh number Nc, the unsteadiness parameter S, the Deborah number of relaxation time  $\alpha_1$ , the Deborah number of retardation time  $\alpha_2$ , the thermal conductivity variable  $\varepsilon_1$ , the solutal diffusivity parameter  $\varepsilon_2$ . These plots are all shown Figs. 2–15.



Figure 3: f' vs.  $M \& \alpha_1$ 

Fig. 2 explores the effect of mixed convective parameter  $\lambda$  and velocity ratio parameter K vs. the flow of fluid f'. The fluid velocity is raised by enhancing the mixed convection parameter  $\lambda$ . Further from these curves lines it is noticed that the flow of fluid f' also improves for greater velocity ratio parameter K. Fig. 3 is confined to discuss the inspiration of magnetic parameter M and Deborah number of relaxation time  $\alpha_1$  vs. velocity profile f'. The larger magnet parameter M and Deborah number of relaxation to time parameter  $\alpha_1$  diminish the velocity profile. Practically,

a larger magnetic parameter produces the Lorenz forces which cause the diminution in the flow of fluid. Fig. 4 provides the information about the inspiration of the buoyancy ratio parameter Nr and Deborah number of retardation time  $\alpha_2$  across velocity field f'. Velocity field f' declines for the highest estimation buoyancy ratio parameter Nr, while it shows opposite behavior for  $\alpha_2$ . Features of unsteady parameter S and bioconvection Rayleigh number Nc vs. the flow of fluid f'are illustrated in Fig. 5. It is clear that the momentum distribution f' declines with enlarging the variation of unsteadiness parameter S and bioconvection Rayleigh number Nc.



Figure 5: f' vs. S & Nc

The influence of radiation parameter Rd on a thermal profile  $\theta$  in the case of constant wall temperature and prescribed surface temperature is shown in Fig. 6. From this figure, it is seen that temperature distribution  $\theta$  exaggerates with radiation parameter Rd. Fig. 7 is presented to check the effect of the temperature ratio parameter  $\theta_w$  on the temperature profile  $\theta$ . It is witnessed that the temperature profile  $\theta$  boosts up for greater temperature ratio parameter  $\theta_w$ . Fig. 8 is plotted to show the temperature distribution  $\theta$  vs. the variable thermal conductivity  $\in_1$  for both constant wall temperature and prescribed surface temperature. Increasing variable thermal conductivity  $\in_1$ leads to higher temperature distribution  $\theta$ . In Fig. 9, the effect of Prandtl number Pr on the thermal field of species  $\theta$  for both constant wall temperature and prescribed surface temperature is illustrated. Thermal field  $\theta$  reduces with the rise in Prandtl number Pr. Fig. 10 describes the temperature profile  $\theta$  for different values of the thermophoretic parameter Nt. It is seen that the thermal field  $\theta$  increases with enlarging the thermophoresis parameter Nt for both constant wall temperature and prescribed surface temperature. Physically, the thermophoresis forces are developed due to increment in thermophoretic parameter which causes the movement of the tiny-sized nanoparticles from a warm surface to the cold region and thus the enhancement of the temperature field.



**Figure 7:**  $\theta$  vs.  $\theta_w$ 



Figure 9:  $\theta$  vs. Pr

Fig. 11 shows how the mixed convection parameter  $\lambda$  and Brownian motion coefficient *Nb* influence the solutal field of species  $\phi$ . Clearly, increasing mixed convection parameter and Brownian diffusion coefficient diminish the concentration  $\phi$ . Fig. 12 is plotted to elucidate the significance of the Prandtl number and Lewis number against the concentration of species  $\phi$ . It is found that an increment in the Prandtl number *Pr* or Lewis number *Le* depreciates the nanoparticle concentration field  $\phi$  [46,47]. To scrutinize the consequence of velocity ratio parameter *K* and thermophoresis parameter *Nt vs.* volumetric concentration of nanoparticles  $\phi$ , Fig. 13 is designed. It is shown that nanoparticle concentration field  $\phi$  is the rising function of velocity ratio parameter *K* and thermophoresis parameter *Nt*. From Fig. 14 it is noticed that  $\phi$  is an uplifting function of solutal diffusivity  $\in_1$  and Arrhenius activation energy parameter *E*. The significance of the Peclet number *Pe* and the bioconvection Lewis number *Lb* against swimming microorganism field  $\chi$  is depicted in Fig. 15. We can see that the microorganism field  $\chi$  reduces for greater Peclet number *Pe* or bioconvection Lewis number *Lb*.



Figure 12:  $\phi$  vs. Pr & Le



**Figure 15:** *χ vs. Pe* & *Lb* 

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Table 1 displays that drag forces coefficient -f''(0) increases with Nr and Nc, but decreases with  $\lambda$ . Tables 2 and 3 depict that heat rate  $-\theta'(0)$  and local Sherwood number  $-\phi'(0)$  are reduced with growing  $\theta_w$  but rises with Pr. Table 4 displays that the local density number of swimming microorganisms increases with Pe and Lb.

M	λ	Nr	Nc	K	S	-f''(0)
0.1	0.1	0.5	0.5	0.3	0.2	1.0101
0.6						1.1280
1.2						1.2517
0.5	0.2	0.5	0.5	0.3	0.2	1.0914
	0.8					1.0087
	1.6					0.9042
0.5	0.1	0.2	0.5	0.3	0.2	1.09734
		0.8				1.1324
		1.6				1.2456
0.5	0.1	0.5	0.2	0.3	0.2	1.1022
			0.8			1.1723
			1.6			1.2768
0.5	0.1	0.5	0.5	0.2	0.2	1.0980
				0.6		1.00812
				1.2		0.8912
0.5	0.1	0.5	0.5	0.3	0.1	1.0101
					0.5	1.1367
					1.0	0.2648

**Table 1:** Estimations of local skin friction coefficient -f''(0) for different parameters

Table 2:	Outcomes	of local	Nusselt	number $-\theta'(0)$ f	for various	parameters
λ	Pr		Nt	Ri	<i>θ</i>	$-\theta'(0)$

M	λ	Pr	Nt	Bi	$ heta_w$	$-\theta'(0)$
0.1	0.1	2.0	0.3	2.0	0.4	0.8276
0.6						0.8099
1.2						0.7982
0.5	0.2		0.3	2.0	0.4	0.8147
	0.8					0.8228
	1.6					0.8323
0.5	0.1	3.0	0.3	2.0	0.4	0.9107
		4.0				0.9900
		5.0				1.0500
0.5	0.1	2.0	0.2	2.0	0.4	0.8072
			0.8			0.7922
			1.6			0.7199
0.5	0.1	2.0	0.3	1.0	0.4	0.5791
				1.6		0.7388
				2.2		0.8442
0.5	0.1	2.0	0.3	2.0	0.1	0.8809
					0.6	0.7762
					1.2	0.6899

				1	,	1
M	λ	Pr	Nt	Nb	Le	$-\phi'(0)$
0.1	0.1	2.0	0.3	0.2	2.0	1.2414
0.6						1.2149
1.2						1.1869
0.5	0.2	2.0	0.3	0.2	2.0	1.2221
	0.8					1.2342
	1.6					1.2484
0.5	0.1	3.0	0.3	0.2	2.0	1.3630
		4.0				1.4850
		5.0				1.5750
0.5	0.1	2.0	0.2	0.2	2.0	1.4036
			0.8			1.5843
			1.6			3.0875
0.5	0.1	2.0	0.3	0.1	2.0	1.3916
				0.4		1.5979
				0.8		1.8989
0.5	0.1	2.0	0.3	0.2	1.4	1.1997
					1.8	1.2468
					2.2	1.3166
0.5	0.1 0.1	2.0 2.0	<b>0.8</b> <b>1.6</b> 0.3 0.3	<b>0.1</b> <b>0.4</b> <b>0.8</b> 0.2	2.0 1.4 1.8 2.2	1.5843 3.0875 1.3916 1.5979 1.8989 1.1997 1.2468 1.3166

**Table 3:** Outcomes of local Sherwood number  $-\phi'(0)$  for various parameters

Table 4: Outcomes of local microorganism density number  $-\chi'(0)$  for various parameters

М	λ	Nr	Nc	Pe	Lb	$-\chi'(0)$
0.1	0.1	0.5	0.5	0.1	2.0	1.3662
0.6						1.3281
1.2						1.2882
0.5	0.1	0.5	0.2	0.1	2.0	1.3812
			0.8			1.3509
			1.6			1.3387
0.5	0.1	0.5	0.5	0.4	2.0	1.4435
				0.8		2.1046
				1.6		3.0148
0.5	0.1	0.5	0.5	0.1	1.0	0.9147
					1.6	1.1817
					2.2	1.4067
0.5	0.2	0.5	0.5	0.1	2.0	1.3396
	0.8					1.3638
	1.6					1.3924
0.5	0.1	0.2	0.5	0.1	2.0	1.3658
		0.8				1.3368
		1.6				1.2976

### **5** Concluding Remarks

In this paper, we focus on the radiative Oldroyd-B nanofluid over stretchable disk with swimming microorganisms. The behavior of variable thermal and solutal diffusivity is investigated. Salient features of this work are:

- The larger buoyancy ratio parameter reduces the flow of fluid.
- The velocity field is improved by increasing the velocity ratio parameter and mixed convection parameter.
- Larger Deborah number of retardation time enhances the momentum distribution, while it decreases bioconvection Rayleigh number.
- The heat transformation is improved by dissolving nanomaterials in base fluid [48].
- The increment in the temperature ratio parameter boosts the temperature field.
- The concentration of nanoparticles is boosted with increasing thermophoretic parameters and Arrhenius activation energy.
- The concentration of nanoparticles is a decreasing function of the mixed convection parameter and the Lewis number.
- The larger Peclet number and bioconvection Lewis number decline the microorganism field.

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