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REVIEW



Application of Fe-Based Amorphous Alloy in Industrial Wastewater Treatment: A Review

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ABSTRACT

Amorphous alloy (MGs) is a solid alloy with disordered atomic accumulation obtained by ultra-rapid solidification of alloy melt. The atom deviates from the equilibrium position and is in metastable state. Up to now, a large number of MGs have been applied to the treatment of dye and heavy metal contaminated wastewater and ideal experimental results have been obtained. However, there is no literature to systematically summarize the chemical reaction and degradation mechanism in the process of degradation. On the basis of reviewing the classification, application, and synthesis of MGs, this paper introduces in detail the chemical reactions such as decolorization, mineralization, and ion leaching of Fe-based amorphous alloy (Fe-MGs) in the degradation of organic and inorganic salt wastewater through direct reduction or advanced oxidation mechanism. Compared with crystalline materials, the higher reaction rate of Fe-MGs can be attributed to lower activation energy, negative redox potential, loose product layer, and band structure with downward shift of valence band top. Finally, some suggestions and prospects are put forward for the limitations and research prospects of MGs in the environmental field, which provides a new idea for the synthesis of new environmental functional materials.

KEYWORDS

Amorphous alloy; industrial waste water; direct reduction; advanced oxidation; reaction activity

1 Introduction

The problem of environmental pollution has perplexed the development of human society since the industrial revolution, so researchers have never stopped exploring the development and utilization of environmental functional materials. Environmental functional materials are new materials that specifically remove harmful substances according to the types and properties of pollutants in the environment. They have the advantages of high reactive activity, low energy consumption, high repetitive utilization rate, little ecological impact, and even has the function of improving and regulating ecological balance [1]. When this kind of material is applied to the treatment of industrial wastewater, it can effectively reduce the treatment cost, save natural resources, and reduce the secondary pollution to the environment. At present, common environmental functional materials can be divided into the following three categories [2]: (1) Production waste. For example, steel slag, fly ash and iron filings in industrial production, and biochar materials prepared from potato slag, rice husk, and straw in agricultural production. (2) Natural minerals. Bentonite, red clay, and attapulgite, etc. (3) Nanomaterials. Nano-sized zero-valent iron, carbon



nanotubes, graphene, and carbon-supported nano- TiO_2 and so on. Among them, production waste and natural minerals are the main parts of traditional environmental functional materials, although the cost is low, but there are some shortcomings such as poor treatment effect and low recycling utilization. Therefore, researchers try to find new materials with low production cost and high reaction activity from other functional materials.

MGs (Fig. 1) is a solid alloy with disordered atomic packing structure, which is obtained when the atoms of the alloy melt are not arranged and crystallized in time during rapid solidification. The internal microparticle arrangement is not periodic, and there is no grain and grain boundary of the crystalline alloy. Compared with the crystalline alloy with regular arrangement of atoms, MGs is a complex structure of many-body interaction. The reason is the particularity of atomic and electronic structure, the whole system is in a thermodynamically metastable state and has higher Gibbs free energy [3]. This special structure makes it have the following properties different from traditional alloy materials: (1) Mechanical properties. Compared with ordinary crystalline alloys, amorphous alloys have no microstructure defects during solidification, so the bonding between atoms is stronger than that of crystalline alloys. In addition, the atoms arranged uniformly and closely together make the amorphous alloy not easy to slip under stress. These factors make the amorphous alloy have good mechanical properties and can be regarded as one of the structural materials with the highest strength. The Co-Fe-Ta-B bulk amorphous alloy developed by Inoue et al. [4] is the metal material with the highest strength at present, and its compressive strength reaches 5185 MPa. (2) Magnetic properties. MGs have a higher saturation magnetic induction compared to their crystalline counterparts. Therefore, their soft magnetic properties are better than those of traditional magnetic materials such as silicon steel, ferrite, and Fe-Ni alloy. The application of MGs to transformers can greatly improve the efficiency, reduce the volume, reduce the weight, and reduce the energy consumption of transformers. At present, there are three kinds of mature amorphous soft magnetic alloys: Fe-based, Co-based, and Fe-Ni-based. They all have excellent soft magnetic properties and can be widely used in the field of power electronics as high-frequency transformers, sensors, and chokes. (3) Electrical properties. Due to the addition of metal-like elements and the chaotic arrangement of atoms, MGs have a strong ability to scatter electrons. At room temperature, the resistivity of MGs is about 100–300 $\mu\Omega$ · cm, while the resistivity of the crystalline allow with the same composition is 1/3-1/2 times lower than that of the same composition [5]. Based on the above excellent properties, MGs have become a new functional material with great research value.



Figure 1: Schematic diagram of MGs structure

In the early 1980s, MGs began to be used in the field of catalysis [6]. In recent years, researchers have carried out a large number of applied and theoretical studies on the catalytic degradation of environmental pollutants by MGs. In the experiment of treating dye wastewater, it is found that MGs have higher reaction

rate and degradation rate than crystalline alloy [7]. The results of theoretical analysis show that MGs with abundant active sites, which can be attributed to the crystal structure dislocations, distortions, and impurities such as metals and metal-like elements caused by the accumulation of disordered atoms [8]. Secondly, the single-phase property of MGs is conducive to the uniform dispersion of reactants on its surface, forming a chemically homogeneous environment, and the high reaction activity is also attributed to the high concentration of unsaturated coordination atoms on the surface [9]. In addition, the element composition and atomic ratio of MGs can be widely adjusted according to the nature of pollutants and treatment environment [10]. Common MGs in the field of water treatment can be divided into the following categories: (1) The most widely used Fe-MGs [11]. Fe have the advantages of non-toxic, rich, cheap, and spontaneous reduction process, so it is an effective reducing agent in the removal of oxidizing pollutants. Single element iron can not form amorphous structure. In order to improve the glass forming ability and thermal stability, a small amount of other metals or metal-like elements are added to Fe to form alloys, such as Fe-B, Fe-Si-B, Fe-Si-B-P and so on. These elements have the advantages of low price and little harm to the environment, which reduce the redox potential of Fe-MGs to a certain extent and promote the catalytic degradation reaction. Based on the above advantages, Fe-MGs is the most widely used MGs in water treatment. (2) Aluminum-based amorphous alloy (Al-MGs) [12] and magnesium-based amorphous alloy (Mg-MGs) [13] with strong reducibility. Because the standard redox potentials of Al and Mg are -1.66 V and -2.37 V, respectively, they show higher reaction activity than Fe-MGs in the reaction with pollutants. However, the price of the main elements Al and Mg is much higher than that of Fe, which is limited in large quantities of water treatment applications. (3) Copperbased amorphous alloy (Cu-MGs) [14] and nickel-based amorphous alloy (Ni-MGs) [15] with low metal leaching rate. Although the catalytic activity of this kind of MGs is lower than that of the former two types, it contains Cu and Ni, which reduces the metal leaching rate in the reaction process and reduces the secondary pollution to the water body, which also has research and application value.

This paper collates the literature on the application of iron-based amorphous alloy (Fe-MGs) in the field of industrial wastewater treatment. The chemical reactions occurred in the treatment of wastewater polluted by organic and inorganic salts by Fe-MGs are analyzed systematically. The two degradation mechanisms of direct reduction and advanced oxidation are discussed emphatically. Finally, some reasonable prospects and suggestions are put forward according to the limitations of MGs in the field of environment.

2 Preparation Method of MGs

Since Au-Si amorphous alloy was first prepared by melt quenching method by Klement et al. [16] in 1960, researchers have developed a series of preparation processes of MGs. The remarkable difference between MGs and crystalline alloy lies in the randomness of atomic arrangement. In the cooling stage of alloy preparation, the atoms will be arranged spontaneously from a disordered state to a periodic crystal structure [17]. In the production of MGs, in order to hinder the regular arrangement of atoms into crystals, the commonly used processes include rapid cooling, mechanical alloying, inhibition of nucleation, zone melting, and chemical reduction.

2.1 Rapid Cooling

The rapid cooling technology is to transfer the heat of the melt to the cooling medium quickly through the contact between the high temperature melt and the low temperature and high thermal conductivity medium, so as to achieve the purpose of cooling the alloy melt very rapidly. the commonly used methods are single roll strip casting, copper mold casting, and gas atomization.

2.1.1 Single Roll Strip Casting

Single roll strip casting is the main method to prepare strip MGs. The structure of the single roll strip casting machine is shown in Fig. 2. When the high frequency current flows through the water-cooled

copper tube coil made into a ring, there is a strong magnetic beam with instantaneous polarity change, which will run through the whole alloy to be heated, thus inducing a strong eddy current. Due to the existence of alloy resistance will produce Joule heat, so that the alloy temperature rises rapidly to melt. By controlling the pressure difference inside and outside the quartz tube, the melt is sprayed into a high-speed rotating copper roller or mold, thus the preparation of a non-equilibrium ribbon with a thickness of 10–70 μ m is realized [18,19]. The technology of single-roll strip spinning has been fully mature and industrial production has been realized, especially the Fe-MGs produced by this method is the main raw material of amorphous core in transformer [20]. At the same time, it also provides a material guarantee for the application of MGs as an environmental functional material in the field of catalytic degradation.



Figure 2: Process flow chart of single roll strip casting

2.1.2 Copper Mold Casting

The size of MGs is limited by the ability of amorphous forming. Copper mold casting is usually used to produce bulk MGs with strong amorphous forming ability. As shown in Fig. 3, the master alloy is heated by an induction coil to make it melt in the quartz tube. Then in an inert atmosphere, the molten alloy liquid is injected into copper by means of blow casting, suction casting and extrusion. Because of the high thermal conductivity of the copper mold, the melt can be cooled quickly, and the bulk amorphous alloy is prepared [21]. In order to make the melt cool quickly in a short time, the volume of the copper mold should be large enough. The copper mold can be water-cooled or not water-cooled. The shapes of copper molds can be divided into wedge-shaped, trapezoidal, rod-shaped and square-shaped. The advantage of copper mold casting is that it is easy to operate and can prepare bulk amorphous alloys of various shapes. The disadvantage is that when the copper mold is used for cooling, the cooling rate is limited $(10-10^3 \text{ K/s})$, and the size of the prepared bulk amorphous alloy is usually small, so it is difficult to achieve large-scale and industrial production. Generally, it is mostly used for laboratory research [22].



Figure 3: Process flow chart of copper mold casting

According to the different atomization medium used, the atomization powders are divided into air atomization and water atomization, which is mainly used to prepare fine powder MGs. The preparation process is that the liquid metal is sheared by high-speed air flow or water flow in the atomization chamber, the kinetic energy of the atomized medium is converted into the surface energy of the liquid metal, and the liquid metal is divided into micron droplets. The process is shown in Fig. 4. The amorphous structure is formed because the droplet size is small and it is easy to obtain a higher cooling rate during the cooling process [23,24]. Chang et al. [25] compared the properties of $Fe_{76}Si_9B_{10}P_5$ Febased amorphous alloy powders prepared by water atomization and gas atomization. The results show that the composition of the powders prepared by the two methods is uniform and the amorphous structure is obvious. Compared with the gas atomized powders, the water atomized powders are more dispersed and the sphere are more regular. The saturation magnetization of the two kinds of amorphous powders are similar, but the coercivity of water atomized powders are lower. The above results show that the performance of $Fe_{76}Si_9B_{10}P_5$ amorphous powders prepared by water atomization method are better than that of gas atomization powders. Compared with ribbon and block MGs, powdered MGs have higher specific surface area in the reaction with pollutants. However, the whole process of atomization is a very complex physical and chemical process, and there is little theoretical guidance in this field. Moreover, the long time interval of nebulizer replacement, the non-uniform design standard, and the high research cost restrict its development in the metal powder production industry. In recent years, with the continuous improvement of the production process of liquid metal pneumatic atomization, coupled with the further study of the mechanism of gas atomization, the technology of metal pneumatic atomization will be continuously improved.



Figure 4: Process flow chart of gas atomization

2.2 Mechanical Alloying

The method of preparing MGs by mechanical alloying is to make the material deform, break and cold weld repeatedly through the collision and friction between the alloyed material and the hard steel ball in the high energy ball mill for a long time, so as to improve the atomic mobility and dislocation density at the interface of the material until the crystal structure is completely lost (Fig. 5). The ball-milled powders have rough surface, irregular shape, larger specific surface area and higher catalytic efficiency than atomized powders [26,27]. In addition, the residual stress in the ball-milled powders will lead to the increase of free energy, thus further improving the catalytic activity [28]. In order to obtain amorphous powders with small particle size and rough surface, the researchers combined gas atomization method with mechanical alloying method. For example, Surreddi et al. [29] first prepared Al₈₄Gd₆Ni₇Co₃ amorphous powders by gas atomization method, and then the powders were milled for different time. It is found that the original crystal phase is amorphized. At the same time, the regular spherical structure

disappears and presents an irregular rough surface. With the extension of ball milling time, the initial crystallization temperature of amorphous increases while the crystallization temperature of intermetallic phase decreases, and the hardness of the powders increase obviously. The production of MGs by mechanical alloying has the advantages of simple technological process, low equipment requirements, and high yield. The disadvantage is that the production cycle is long, the loss of equipment is serious, and the output is small. Therefore, it is not suitable for industrial production and is mainly used for laboratory research.



Figure 5: Schematic diagram of mechanical alloying

2.3 Inhibition of Nucleation

The inhibition of nucleation is mainly the inhibition of heterogeneous nucleation. In the alloy design and equipment selection, attention should be paid to improving the purity of the material, doping the secondary elements which are quite different from the atomic size of the main elements, and the crystal structure of the selected cooling medium is quite different from that of the crystal nucleus [30]. The commonly used methods are tube drop method, molten glass purification method and suspension melting method [31]. These methods are to reduce the contact between the melt and the container in the cooling process, avoid heterogeneous nucleation and improve the amorphous forming ability of the material.

2.4 Zone Melting

The above methods are all segmented operation, and the material size is small, so it is not suitable for the production of large parts and materials. For this reason, the zone melting technology (Fig. 6) is developed to produce rod-like MGs. The rod-like alloy material is placed in the groove of water-cooled copper die, and the material is melted by high-energy heat source. At the same time, the relative motion between the copper mold and the heat source causes the rapid movement of the solid-liquid interface. The huge temperature gradient between the melting zone and the solid zone rapidly cools the melting zone to form an amorphous structure [32]. This process has been widely used in industrial production. The size of rod-shaped MGs prepared by this process can reach $200 \times 10 \times 10$ mm.

2.5 Chemical Reduction Method

The chemical reduction method is to use the reducing agent containing metal-like metal (KBH₄ or NaH₂PO₂) to drop into the metal salt solution, so that the metal ion is reduced to metal, and then the metal particles are repeatedly leached and dried to obtain nano-sized amorphous particles. The preparation parameters such as pH value of solution, metal elements, ratio of reactants and temperature have important effects on the microstructure and catalytic performance of MGs. Compared with other

processes mentioned above, the preparation conditions of the chemical reduction method are mild, the morphology of the nanoparticles can be controlled and the composition of the alloy is not limited by the eutectic composition, and the atomic ratio can be changed arbitrarily [33]. This method has been widely used in the production of nanometer amorphous catalysts.



Figure 6: Schematic diagram of zone melting method

3 Treatment of Dye Wastewater by MGs

In recent years, the annual output of the global synthetic dye market has exceeded 10 million tons and continues to grow at a rate of 3–4%. At the same time, the production and use of dyes are accompanied by energy consumption and environmental pollution. According to the investigation, about 744 L of waste water is discharged to the environment for each production of 1 kg synthetic dyes [34,35]. Dyeing 1 kg cotton requires 30–60 g dyes and 70–150 L water, of which 10–20% of the dyes are indirectly released into the environment because they cannot be fully utilized [36]. The dyes are mainly composed of polyphenylene ring substituted compounds and heavy metal salts such as lead, arsenic, chromium, mercury and so on. Once this kind of highly toxic, high chromaticity and refractory substances enter the water ecosystem, it will cause serious damage to the ecological balance. Therefore, the reasonable treatment of dye wastewater can not only reduce the harm to the environment and protect human health, but also reuse the purified water and save limited water resources, which is in line with the sustainable development strategy advocated all over the world.

3.1 Decolorization Reaction

The ability of dyes to show different colors is based on the conjugated systems such as azo bond and nitrogen-oxygen bond in dye molecules. When visible light is irradiated on the dye, the conjugated system can selectively absorb specific wavelength energy. The light in other bands is reflected and presents different colors [37]. The decolorization reaction of MGs with organic dyes is to destroy the chromophoric groups such as C=O, -N=N-, -NO₂, and -N=O, which can be used as chromogenic groups. The results show that the chromaticity removal rate of MGs for commonly used dye-contaminated wastewater is close to 100%. For example, Jia et al. [38] developed a multi-component Fe₈₃Si₂B₁₁P₃C₁^{AR} catalyst using arc melting and melt spinning technology to treat mixed aqueous solutions containing rhodamine B, methylene blue, methyl orange, and complex organic structures. As shown in Fig. 7, the solution is gradually decolorized to colorless within 30 min. The decolorization rate of the above four different organic wastewater is 100%. By comparing the degradation rates of the three dyes, it is found that the degradation rate of methylene blue with amino group by Fe₈₃Si₂B₁₁P₃C₁^{AR} is the fastest, methyl orange with azo bond as chromophore is the second, and rhodamine B with phenylamino group and carbonyl group as chromophore is the slowest. This shows that the different functional groups in the dyes

have a direct effect on the decolorization reaction. Xie et al. [39] compared the decolorization performance of methyl orange wastewater by $Fe_{76}B_{12}Si_9Y_3^{AR}$ and crystalline zero-valent iron (ZVI). After 1 h, the wastewater treated by $Fe_{76}B_{12}Si_9Y_3^{AR}$ lost color completely, while the wastewater treated by ZVI still had high chromaticity. In order to understand the degradation process, the mass spectrometric analysis of the intermediate products is shown in Fig. 8. Methyl orange is first decomposed into N-dimethylaniline, N-dimethyl-p-phenylenediamine, and sulfonamide, followed by further degradation into small molecular organic compounds such as benzenesulfonic acid, and partially decomposed into carbon dioxide and water. The authors believe that the excellent properties of $Fe_{76}B_{12}Si_9Y_3^{AR}$ are mainly due to the heterogeneous structure composed of local iron-rich and poor iron clusters, rather than the large specific surface area and strong residual stress of the powders. Table 1 shows the decolorization rate of some MGs to dye wastewater.



Figure 7: The color change (a) and decolorization rate (b) of rhodamine B, methylene blue, methyl orange and mixed dyes degraded by $Fe_{83}Si_2B_{11}P_3C_1^{AR}$ [38]

3.2 Mineralization Reaction

The chromaticity of dyes can reflect the content of dyes in solution to a certain extent, but the decrease of chromaticity does not prove that dyes are completely decomposed, only that the chromophoric groups in dye molecules are destroyed [47]. In order to more accurately reflect the performance of MGs in the degradation of dyes, the researchers proposed to use organic carbon content (TOC) to measure the degree of mineralization of polymer dyes into small molecules such as CO_2 , H_2O , and inorganic salts [48]. Jia et al. [49] used $Fe_{78}Si_9B_{13}^{AR}$ to treat brilliant red 3B-A solution, most of the dyes can be degraded into inorganic salts such as H_2O , CO_2 , NO_3^- , and SO_4^{2-} within 5 min, and the final removal rate of TOC can reach 80%. However, due to the existence of Cu and Nb, $Fe_{73.5}Si_{13.5}B_9Cu_1Nb_3^{AR}$ is difficult to form pores on the surface of the strip, so the reaction activity is reduced, the reaction time is extended to 30 min, and the removal rate of TOC is reduced to 65%. Table 2 lists several MGs removal rates of TOC in dye wastewater.

3.3 Leaching Reaction

Ions are inevitably released into the water during the reaction between MGs and pollutants, which not only causes secondary pollution to the environment, but also reduces the recycling utilization of the catalyst. There are two main sources of leaching ions: (1) After the molecular structure of the dye is destroyed, the

metal ions contained in it break away from the bulk structure and enter into the solution. (2) The redox reaction occurs between MGs and dyes, and part of MGs loses electrons and is leached in solution. It is difficult to reduce the amount of ions released from dye molecules in the process of degradation, so it is necessary to reasonably design the structure and composition of MGs to reduce the leaching of catalysts. On the one hand, choose metals and metal-like elements that have no pollution to the environment, such as Fe, Si, B and so on. On the other hand, corrosion resistant elements such as Ni, Nb are added to it. In order to reduce the leaching rate of MGs, Liang et al. [51] doped 3% Nb into the alloy, the initial dosage of Fe_{73.5}Si_{13.5}B₉Cu₁Nb₃^{AR} was 2 g/L, and the leaching amounts of Fe and Si after reaction with malachite green are 28 mg/L and 0.05 mg/L, respectively. Wang et al. [53] obtained that the leaching amount of Fe after the degradation of methylene blue by Fe₇₈Si₉B₁₃^{AR} is only 26 mg/L, and the SiO₂ attached to the surface of the strip after the reaction played a role in reducing the leaching of the catalyst to a certain extent. Some scholars believe that the proper leaching of non-toxic ions can improve the electrical conductivity of the solution and promote the electron transfer on the interface of MGs, thus improving the degradation rate of pollutants [52].



Figure 8: The ion spectra of full-scan products at different times. (a) start time; (b) reaction 10 min; (c) reaction 24 h; (d) product formation sequence [39]

MGs (^{AR} is ribbon, ^{AP} is powder)	Preparation method	Dye	Initial dye concentration/mg/L	Time/ min	Decolorization rate/%	Reference
Fe78Si9B13 AR	Single roll strip casting	Orange II	40	70	100	[40]
$\mathrm{Fe_{78}Si_8B_{14}}^{\mathrm{AR}}$	Single roll strip casting	Orange II	100	30	100	[41]
$Fe_{80}P_{13}C_7^{AR}$	Melt spinning	Methylene	100	17	100	[42]
		blue				
$Fe_{83.3}Si_4B_8P_4Cu_{0.7}^{AR}$	Melt spinning	Methyl orange	20	40	100	[43]
$Fe_{72}Si_2B_{20}Nb_6^{\ AR}$	Melt spinning	Direct blue 15	50	60	100	[44]
$\mathrm{Fe_{78}Si_9B_{13}}^{\mathrm{AR}}$	Single roll strip casting	Acid Orange II	200	60	100	[45]
Fe ₇₈ Si ₉ B ₁₃ ^{AP}	Gas atomization	Direct blue 6	200	10	98	[46]

Table 1: Decolorization rate of dye wastewater by MGs

Table 2: Removal rate of TOC in dye wastewater by several kinds of MGs

MGs	Preparation method	Dye	Time/ min	Removal rate of TOC/%	Reference
Fe ₇₈ Si ₉ B ₁₃ ^{AR}	single roll strip casting	Congo red	60	80	[50]
Fe _{73.5} Si _{13.5} B ₉ Cu ₁ Nb ₃ ^{AR}	Melt spinning	Malachite green	30	55	[51]
Fe ₇₈ Si ₉ B ₁₃ ^{AR}	single roll strip casting	Methylene blue	30	60	[52]
$Fe_{83}Si_2B_{11}P_3C_1^{AR}$	Melt spinning	Rhodamine B	30	50	[38]
		Methylene blue	5	60	
		Methyl orange	30	63	
		Mixed dye	15	55	

4 Treatment of Inorganic Salt Wastewater by MGs

Based on the efficient degradation of organic dyes by MGs, in recent years, researchers have applied it to the treatment of wastewater polluted by heavy metals, metal-like and inorganic acid ions and achieved good results. Yan et al. [54] used $Fe_{78}Si_9B_{13}^{AR}$ to treat wastewater polluted by Cu^{2+} ions. The initial concentration of Cu^{2+} ions was 500 mg/L, and the dosage of ribbon was 2 g/L. After 60 min of reaction, the concentration of Cu²⁺ ions decrease to 1 mg/L, and the color of the solution change from light green to colorless. The Fe in the ribbon reacts with the Cu^{2+} ions in the solution (as shown in Fig. 9), and the Cu^{2+} ions is precipitate from the solution in the form of copper. The reaction rate constant obtained by fitting the quasi-first-order kinetic equation is 0.0667 min^{-1} . However, under the same reaction conditions, the rate constant of the reaction of ZVI with Cu^{2+} ions is 0.0344 min⁻¹. For the reason why $Fe_{78}Si_9B_{13}^{AR}$ can efficiently reduce Cu^{2+} ions, Zhang et al. [55] observed by SEM that there is a great difference in the structure and morphology between the amorphous bands and the surface products of ZVI. As shown in Fig. 10, the product layer on the surface of the amorphous ribbons has a pore structure perpendicular to the reaction interface, which is beneficial to the diffusion of Cu^{2+} ions to the reaction interface. However, the product laver of ZVI is irregularly arranged in the dendritic shape, which closely covers the surface of ZVI and hinders the transmission of Cu^{2+} ions, which is one of the reasons for the low activity of ZVI reaction. Liang et al. [56] remediated groundwater contaminated by As^{5+} ions and NO_3^{-} ions by reductive precipitation. When $Fe_{78}Si_9B_{13}^{AR}$ and Na_2S were added to the polluted groundwater at the same time, $Fe_{78}Si_9B_{13}^{AR}$ reduced As^{5+} ions to As^{3+} ions and then combined with S^{2-} ions to form As_2S_3 precipitation. The maximum amount of As^{5+} ions removal is up to 95% at 25°C. NO_3^- can be removed from aqueous solution in three ways: (1) under acidic conditions, NO_3^- is reduced by iron to NH_4^+ (Eq. (1)). (2) NO_3^-

is reduced to N_2 and OH^- by Eq. (2), (3) The generated Fe^{2+} ions is oxidized to Fe^{3+} ions and then combined with OH^- to form $Fe(OH)_3$ with water purification function (Eq. (3)). The unreduced NO_3^- is removed from the water by $Fe(OH)_3$ adsorption. The ribbons still maintained high reaction activity after being reused for 20 times. At present, the research on the treatment of inorganic salt wastewater by MGs is less and the type of ions is single, so it needs to be further explored in the future.

$$4Fe + NO^{3-} + 10H^+ \rightarrow 4Fe^{2+} + NH^{4+} + 3H_2O$$
(1)

$$5Fe + 2NO^{3-} + 6H_2O \rightarrow 5Fe^{2+} + N_2 + 12OH^-$$
 (2)

$$4Fe^{2+} + 8OH^{-} + O_2 + 2H_2O \rightarrow 4Fe(OH)_2$$
(3)



Figure 9: $Fe_{78}Si_9B_{13}^{AR}$ treatment of Cu^{2+} contaminated wastewater: (a) color change; (b) reaction mechanism [54]

5 Degradation Mechanism

The degradation mechanism of pollutants by Fe-MGs can be divided into two kinds: one is to make use of the electronegativity of ZVI to reduce the pollutants directly to achieve the purpose of degradation. The other is to produce strong oxidizing hydroxyl radical ·OH by fenton method to oxidize and remove the pollutants. Fig. 11 shows the reaction process of the two degradation mechanisms.

5.1 Direct Reduction

The redox reaction is easy to occur, which requires the reductant to have a negative electrode potential and the oxidant to have a positive electrode potential. The standard electrode potential of Fe is -0.44 V, which has good reducibility in the removal of organic matter and oxidizing pollutants. As shown in Eqs. (4)–(11), When Fe comes into contact with pollutants, it is easy to lose electrons and convert them into Fe²⁺ or Fe³⁺ ions. The electrons generated are captured by organic compounds or heavy metal salts to reduce and degrade the pollutants. In addition, Fe reacts with H₂O or H⁺ ions to form an active hydrogen atom [H], which has a strong reducibility, resulting in the breaking of the chemical bond (-N=N-) in the molecules of organic pollutants [57]. Therefore, as a traditional environmental functional material, ZVI have been widely used in the treatment of groundwater or industrial wastewater.

$$\mathrm{Fe}^0 \to \mathrm{Fe}^{2+} + 2\mathrm{e}^- \tag{4}$$

$$\mathrm{F}\mathrm{e}^{2+} \to \mathrm{F}\mathrm{e}^{3+} + \mathrm{e}^{-} \tag{5}$$

$$2H_2O(1) + 2e^- \rightarrow H_2(g) + 2OH^-(aq)$$
 (6)

$$H_2O(l) \to H^+(aq) + OH^-(aq)$$
⁽⁷⁾

$$\mathrm{H}^{+}(\mathrm{aq}) + \mathrm{e}^{-} \to [\mathrm{H}] \tag{8}$$

$$[H] + [H] \rightarrow H_2(g) \tag{9}$$

$$R - N = N - R' + 4H + (aq) + 4e^{-} \rightarrow R - NH_2 + R' - NH_2$$
(10)

$$R - N = N - R' + 4[H] \rightarrow R - NH_2 + R' - NH_2$$
 (11)



Figure 10: The product morphology of $Fe_{79}Si_{13}B_8^{AR}$ and ZVI: (a) $Fe_{79}Si_{13}B_8^{AR}$; (b) is the high resolution map of b region in (a); (c) ZVI; (d) is the high resolution map of d region in (c) [55]

Fe-MGs is a special kind of ZVI, in order to compare the difference between Fe-MGs and ZVI in the treatment of pollutants, some researchers have carried out the kinetic analysis of the reaction process. Tang et al. [58] used amorphous ribbons $Fe_{86}B_{14}^{AR}$, crystalline ribbons $Fe_{86}B_{14}^{CR}$, and ZVI to degrade Direct Blue 6 under the same external conditions. The apparent reaction rate constant k_{obs} was obtained by fitting the quasi-first-order kinetic equation (Eq. (12)). It is found that the k_{obs} of $Fe_{86}B_{14}^{AR}$ in the degradation reaction is 1.8 and 89 times higher than that of $Fe_{86}B_{14}^{CR}$ and ZVI, respectively, indicating that the catalytic rate of amorphous materials is higher than that of crystalline materials. In addition, the formation of oxide layer can be controlled by fine-tuning the content of B, which can further improve the catalytic efficiency of Fe-B amorphous ribbons. On this basis, Tang et al. [59] further explored the degradation process of orange II by ternary amorphous ribbons $Fe_{79}Si_{13}B_8^{AR}$ and ZVI. Using Arrhenius

formula (Eq. (13)), the apparent activation energy ΔE of $Fe_{79}Si_{13}B_8^{AR}$ is 17.98 kJ/mol, and that of ZVI is 31.98 kJ/mol. Therefore, $Fe_{79}Si_{13}B_8^{AR}$ is more likely to be excited to change from a conventional state to an active state capable of chemical reaction. Fig. 12 compares the ΔE of Fe-MGs and ZVI in the degradation of typical azo dyes acid orange (a) and direct blue 6 (b). For the same dye, the ΔE of all Fe-MGs is lower than that of ZVI, indicating that Fe-MGs in metastable state have higher reaction activity than crystalline ZVI, which are more suitable to be used as environmental functional materials in the field of water treatment. In order to show that Fe-MGs generally have higher k_{obs} and lower ΔE in catalytic reaction, the kinetic parameters of catalytic degradation of various dyes by different Fe-MGs are summarized in Table 3.

$$\ln(C_{\rm t}/C_0) = -k_{\rm obs} \cdot t \tag{12}$$

$$\ln k_{\rm T} = \Delta E/{\rm R}T + \ln{\rm A}$$



Figure 11: Reaction process of reduction and oxidation mechanism



Figure 12: ΔE in the degradation of acid orange (a) and direct blue 6 (b) by Fe-MGs and ZVI [38,58–60]

The above results explain why MGs have higher catalytic activity than crystalline materials from the point of view of kinetics, but it is still at the apparent level. Through the redox potential of MGs in dye wastewater, some researchers explained the deep reason why the k_{obs} of MGs is higher and ΔE is lower. Weng et al. [64] measured that the redox potentials of Fe₈₅B₁₅^{AP} and Fe₇₆Si₉B₁₀P₅^{AP} in methyl orange solution are -0.47 V and -0.45 V, respectively, which are lower than the redox potential of ZVI -0.437 V. Therefore, Fe₈₅B₁₅^{AP} and Fe₇₆Si₉B₁₀P₅^{AP} have stronger reductivity. Zhang et al. [55] measured

(13)

the potentiodynamic polarization curves of pure iron strips and Fe-Si-B amorphous strips in CuSO₄ solution. The electrode potential of Fe-Si-B amorphous ribbons is lower than that of pure iron ribbons due to the presence of non-metallic elements Si and B in the amorphous ribbons. This result also explains the inherent reason why the k_{obs} of the reaction of Fe-Si-B amorphous ribbons with Cu²⁺ ions is higher than that of ZVI. In order to determine whether the atomic disorder stacking structure in MGs is one of the reasons for the decrease of redox potential, Tang [60] measured the open circuit potential of Fe₇₈Si₉B₁₃^{AR}, Fe₇₈Si₉B₁₃^{CR}, and ZVI in methyl orange wastewater under the same external conditions as -0.735 V, -0.471 V, and -0.439 V, respectively. Comparing the open circuit potential of Fe₇₈Si₉B₁₃^{CR}, it is found that the open circuit voltage of the alloy with the same nominal composition is different due to the different arrangement of internal atoms. Therefore, it can be determined that the disorder stacking structure of atoms in MGs is one of the reasons for the decrease of redox potential.

Table 3: The k_{obs} and ΔE in the degradation of dyes by Fe-MGs

MGs	Dye	Temperature/ K	k _{obs} / min ⁻¹	ΔE/kJ/ mol	Control steps	Degradation rate/%	Reference
Fe ₇₈ Si ₉ B ₁₃ ^{AR}	Acid orange II	298	0.174	35.9	Surface	96.7	[61]
		303	0.205		control		
		313	0.299				
		323	0.412				
$(Fe_{0.99}Mo_{0.01})_{78}Si_9B_{13}^{AR}$	Acid orange II	298	0.168	28.4	Diffusion	97.8	[62]
		303	0.185		control		
		313	0.282				
		323	0.407				
$Fe_{63}Cr_5Nb_4Y_6B_{22}{}^{AR}$	Methylene blue	283	0	21.8	Diffusion	95.0	[63]
		303	0.087		control		
		323	0.182				
		343	0.239				
Fe ₇₆ Si ₉ B ₁₀ P ₅ ^{AP}	Methyl orange	298	0.151	19.5	Diffusion control	96.0	[64]
		308	0.196				
		318	0.251				
		328	0.298				
	Direct blue 6	298	0.241	26.8	Diffusion control	97.6	
		308	0.297				
		318	0.346				
		328	0.388				

Note: ΔE in the range of 8–21 kJ/mol is controlled by diffusion in solution, and $\Delta E > 29$ kJ/mol is controlled by surface control [65].

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When Fe-MGs degrades pollutants through direct reduction mechanism, the Fe in Fe-MGs loses the outermost electrons as a reducing agent. From the analysis of the above experimental results, it is found that Fe-MGs have higher reducibility than the same component crystalline alloy and ZVI, that is, the outermost electrons of Fe-MGs are easier to break away from the binding force of the nucleus and transfer to the contaminants. In order to compare the electron loss ability of amorphous and crystalline materials, Zhang et al. [66] analyzed the valence band densities of states of $Fe_{78}Si_8B_{14}^{AR}$ and ZVI by X-ray photoelectron spectroscopy as shown in Fig. 13. There is an obvious difference in the energy band structure between the two materials. The valence band top of $Fe_{78}Si_8B_{14}^{AR}$ is 0.16 eV lower than that of ZVI, and the empty band is widened accordingly, which makes it easier for electrons in 4 s orbitals to overcome the energy barrier and be activated into the empty band. Therefore, in the process of reductive degradation of dyes, $Fe_{78}Si_8B_{14}^{AR}$ can provide more excited electrons to participate in the catalytic reaction. The simple disordered stacking of atoms can make the electrons get rid of the constraints of the lattice, which shows the superiority of MGs structure.



Figure 13: (a) Total Valence Band density of States of ZVI and $Fe_{78}Si_8B_{14}^{AR}$; (b) Schematic diagrams of different electronic structures of ZVI and $Fe_{78}Si_8B_{14}^{AR}$ [66]

5.2 Advanced Oxidation

Advanced oxidation is a new purification technology for oxidative degradation of organic pollutants, which mainly includes ozonation, photocatalysis, and fenton method [67,68]. Iron-based materials are mainly oxidized and degraded by fenton method. The principle is that Fe^{2+} ions reacts with fenton agent H_2O_2 to form strong oxidizing \cdot OH (formula 14), and its redox potential can reach 2.7 V. The generated \cdot OH can quickly oxidize and decompose organic pollutants into CO_2 , H_2O , and inorganic small molecular substances. During this process, when Fe^{2+} ions is converted to Fe^{3+} ions, it cannot continue to generate \cdot OH. Moreover, Fe^{3+} ions can also consume H_2O_2 to produce HO_2 with negative redox potential (Eq. (15)), which seriously inhibits the oxidative decomposition of organic pollutants. At this time, if there is ZVI in the solution, the generated Fe^{3+} ions can be reduced to Fe^{2+} ions again (Eq. (16)) to participate in the formation of OH. The traditional ZVI is easy to be passivated due to the adhesion of the reaction products on its surface, which reduces the long-term reaction activity of ZVI. Using Fe-MGs instead of ZVI can effectively alleviate the passivation phenomenon on the surface of the material and reduce the amount of catalyst.

$$Fe^{2+} + H_2O_2 \rightarrow Fe^{3+} + OH^- + OH$$
(14)

$$Fe^{3+} + H_2O_2 \to Fe^{2+} + HO_2 \cdot + H^+$$
 (15)

$$Fe + 2Fe^{3+} \rightarrow 3Fe^{2+} \tag{16}$$

As the effect of fenton reaction on the degradation of pollutants is greatly affected by the external environment, some researchers explore the best process parameters under different experimental conditions. Wang et al. [69] studied the effects of temperature, pH, and H_2O_2 concentration on the degradation of rhodamine B. The results show that the complete degradation of rhodamine B can be achieved in about 10 min by adding 0.5 g $Fe_{78}Si_9B_{13}^{AR}$ catalyst and 1.6 mol/L H_2O_2 to the solution of rhodamine B at the temperature of 295 K and pH = 3 and the concentration of 20 mg/L. The degradation process accords with the description of pseudo-first-order kinetic model. The strips still have good structural stability after being reused for three times, and there are no obvious performance loss. The most direct factor affecting the efficiency of oxidative degradation is the amount of OH. Properly increasing the amount of catalyst and H₂O₂ is helpful to the rapid formation of ·OH. Jia et al. [49] used Fe₇₈Si₉B₁₃^{AR} and Fe_{73.5}Si_{13.5}B₉Cu₁Nb₃^{AR} as catalysts to degrade brilliant red by fenton. As shown in Fig. 14, with the increase of amorphous ribbons and H₂O₂ content, the rate of catalytic degradation increases and the decolorization rate increases. According to Eq. (17), it can be understood that more effective Fe²⁺ ions can be extracted from the ribbons with higher fenton dosage. However, when the concentration of Fe^{2+} ions in the solution is too high, it will react with OH (Eq. (18)), and the consumption of the resulting ·OH leads to the decrease of degradation efficiency [70].

$$Fe + H_2O_2 = Fe^{2+} + 2OH^-$$
(17)

$$Fe^{2+} + \cdot OH = Fe^{3+} + OH^{-}$$
 (18)



Figure 14: Effect of fenton concentration on decolorization rate of brilliant red 3B-A: (a) $Fe_{78}Si_9B_{13}^{AR}$ and $Fe_{73.5}Si_{13.5}B_9Cu_1Nb_3^{AR}$; (b) H_2O_2 [49]

The fenton system can be carried out spontaneously without external energy. If the external energy can be input in the reaction process, the catalytic performance of the system can be effectively improved. For example, increasing the temperature of the system can significantly increase the reaction rate, because at high temperature, the reactant can easily cross the energy barrier to an active state capable of chemical reaction. At the same time, high temperature is beneficial to the diffusion of matter and accelerate the reaction [69]. Light radiation is also an effective way of energy input. When the fenton system is irradiated with high intensity light, the rate of photochemical reaction of Fe^{3+} ions to Fe^{2+} ions is

accelerated through Eq. (19). This is because the unstable electrons of $4s^2$ orbitals in amorphous Fe atoms are easily activated, resulting in rapid electron transfer [71]. In order to improve the light energy efficiency of MGs, Yang et al. [72] prepared composites MGs/TiO₂ by doping TiO₂ into Fe₇₈Si₉B₁₃^{AP}. Under visible light irradiation, the decolorization rate of methylene blue degraded by TiO₂ is 3 times higher than that of crystalline alloy (CA)/TiO₂ (Fig. 15a). The synergistic strengthening mechanism of MGs/TiO₂ is shown in Fig. 15b. The action mechanism of MGs is similar to that of ZVI, but it has enhanced performance. The catalyst is excited by photons, and the electrons transition from the valence band (VB) of TiO₂ to the conduction band (CB), resulting in electron-hole pairs. The electrons produced by TiO₂ prevent the formation of oxide layer on the surface of metallic glass by reducing Fe³⁺ ions to Fe²⁺ ions.

$$\operatorname{Fe}(\operatorname{OH})^{2+} + \operatorname{hv} = \cdot \operatorname{OH} + \operatorname{Fe}^{2+}$$
(19)



Figure 15: Decolorization rate (a) and reaction mechanism (b) of methylene blue degraded by MGs/TiO₂ [72]

6 Reuse of MGs

Reuse is one of the important indicators of environmental functional materials, which determines whether the materials can be applied in large-scale engineering. Fe-MGs have a good structural stability in the catalytic reaction, and the surface oxide layer is loose and easy to fall off, so it is not easy to passivate, which is conducive to the effective contact between the catalyst and pollutants, so that the catalytic reaction can occur continuously. In order to test the reusable times of Fe-MGs, the ribbons after reaction were filtered from the water after each degradation experiment. Under the premise of not destroying the surface products of the ribbons, the ribbons were washed with deionized water several times in order to remove the contaminants attached to the surface. Then the ribbon was applied to the next batch of degradation experiments and recycled several times until the ribbons lost its degradability. According to the statistics of the current research results (Table 4), Fe-MGs can be reused more than 4 times. The main reasons for the decrease of the catalytic performance of the materials include the following two points: (1) in the process of reductive degradation, a large number of reaction products precipitate many times on the surface of the catalyst, which hinders the diffusion of pollutants to the reaction interface. (2) The repeated contact between Fe-MGs and active substance OH in fenton reaction leads to serious surface oxidation of the catalyst [70]. Therefore, the reuse of H₂O₂ can be improved by controlling the amount of Fe-MGs, ultrasonic vibration and self-updating [53].

MGs	Preparation method	Pollutant	Degradation mechanism	Reuse	Reference
Fe ₇₈ Si ₈ B ₁₄ ^{AR}	Melt spinning	Acid orange II	Hydrogenation reduction	The k_{obs} of the fourth time of recycling is similar to that of the first three times.	[57]
Fe ₇₈ Si ₉ B ₁₃ ^{AR}	Melt spinning	Rhodamine B	Fenton oxidation	After 4 times of recycling, Rhodamine B can still be completely degraded within 10 min.	[69]
Fe ₇₈ Si ₉ B ₁₃ ^{AR}	Melt spinning	Brilliant red 3B-A	Fenton oxidation	The decolorization rate of the fourth recycling is 70% of that of the first.	[49]
$\mathrm{Fe_{78}Si_9B_{13}}^{\mathrm{AR}}$	Melt spinning	Naphthol green B	Fenton oxidation	It is reused 10 times and the decolorization rate is 89.4%.	[73]
Fe ₇₆ B ₁₂ Si ₉ Y ₃ ^{AR}	Melt spinning	Methyl orange	Hydrogenation reduction	The degradation rate remains almost unchanged after recycling for 13 times.	[42]
Fe ₇₈ Si ₉ B ₁₃ ^{AR}	Melt spinning	Methylene blue	Fenton oxidation	After 20 times of recycling, the kobs decreased from 0.718 min ⁻¹ to 0.217 min ⁻¹ , which is still much higher than using persulfate alone.	[52]
Fe ₈₀ P ₁₃ C ₇ ^{AR}	Melt spinning	Methylene blue	Fenton oxidation	The loose cottonlike product layer falls off from the strip, exposing a fresh substrate. Can be reused 19 times.	[53]

Table 4: Reuse of Fe-MGs in different wastewater

7 Conclusion and Prospect

In this paper, the research progress on the functional application of a new environmental functional material Fe-MGs in the treatment of wastewater polluted by organic compounds and heavy metals is reviewed. At present, the most widely studied is the catalytic degradation of azo dye wastewater. The main chemical reactions in the treatment process include decolorization, mineralization, and ion leaching. According to the different electron transfer modes of Fe-MGs, there are two degradation mechanisms. One is that Fe-MGs transfers electrons directly to pollutants for reductive degradation. The other is that Fe-MGs transfers electrons to peroxides to form a strong oxidizing active substance \cdot OH, which is degraded by oxidation mechanism. A large number of comparative experimental results show that the k_{obs} and degradation rate of pollutants treated by Fe-MGs are higher than those of traditional degrader ZVI. This is due to the fact that Fe-MGs have lower apparent activation energy and redox potential than ZVI. Secondly, the downward shift of the valence band top of Fe-MGs makes it easier for electrons to be excited to participate in chemical reactions. By observing the structure of the product layer of the two materials, it is found that the product layer of Fe-MGs have a three-dimensional nano-pore structure and is easy to fall off, which is beneficial to the electron transfer and the diffusion of pollutants to the reaction interface. Although MGs have many excellent properties, there are still some problems in the practical

application of MGs as environmental functional materials in water treatment. For example, the current research mainly focuses on the degradation of a single azo dye, and the results are different from the actual situation. Even under the simplified experimental conditions, the theoretical research is still in the stage of fitting the kinetic and thermodynamic parameters, and the fundamental principle of how the amorphous structure causes the reduction of activation energy and redox potential and the acceleration of reaction rate constant is not clearly explained. In addition, the leaching of metal ions in the degradation process caused secondary pollution to the water. Based on the above problems, researchers should consider carrying out the following aspects of work in the future:

- (1) Expand the application range of MGs in water treatment. MGs are mainly used to treat azo dye wastewater with single kinds of pollutants. Industrial wastewater is a coexistence system of many kinds of pollutants. Therefore, the effect of the interwoven system of heavy metals, toxic metals, and organic compounds on the degradation performance should be considered in the experimental stage.
- (2) Preparation of amorphous composite materials. MGs can control the properties of alloys by changing the type and proportion of atoms, and can also consider the addition of strong conductive materials such as graphene, carbon nanotubes, and biochar to change the electronic conductivity.
- (3) Further improve the theoretical system. The theoretical explanation for the high reactivity of MGs is still at the apparent level, so there is an urgent need to establish the model theory of electron transport behavior and amorphous structure in metastable state, so as to provide theoretical guidance for the design, development and performance improvement of MGs.
- (4) Develop simulation software. Deeply understand the corrosion mechanism of MGs and optimize the design of MGs.

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